



Sous-Station de Réseau de Chaleur

Architecture, Contrôle et Innovation

JEUDI 27 MAI 2021

N. Lamaison

Innovation laboratory for new energy technologies and nanomaterials – www.liten.cea.fr

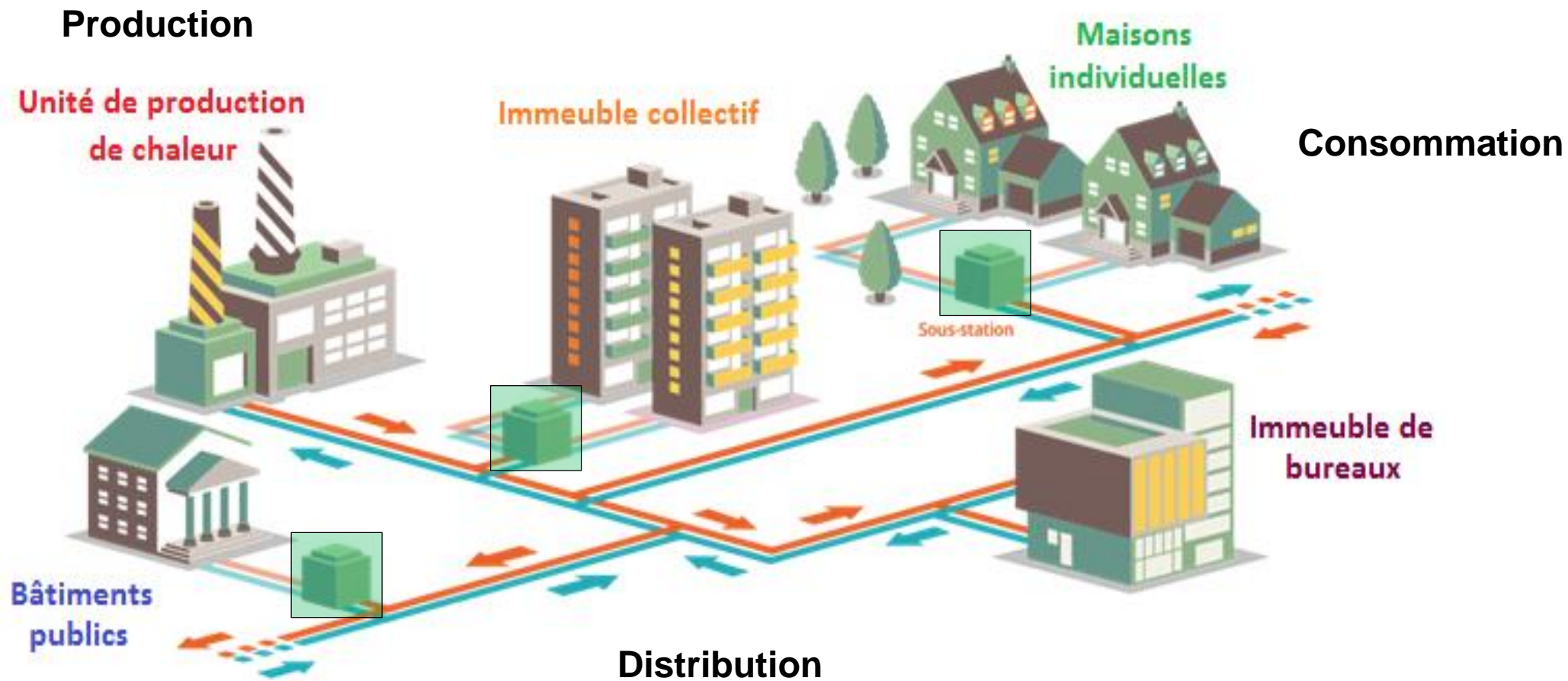
- **Donner un aperçu de la technologie actuelle des sous-stations**
- **Présenter un ensemble de sujets de recherche traités au CEA Liten**

- **Introduction: Généralités sur les réseaux de chaleur et les sous-stations**

- **Architecture et contrôle**
 - Logique de contrôle globale
 - Différentes architectures primaire / secondaire
 - Détaille d'une architecture
 - Equipements
 - Dimensionnement
 - Analyse de données
 - Challenges futurs

- **Innovation**
 - Topic 1: Critical Temperature
 - Topic 2: Prosumer Substation
 - Topic 3: Innovative Design with Primary Storage
 - Topic 4: Advanced Control
 - Topic 5: Flat Substation
 - Topic 6: Faults detection in substation

GÉNÉRALITÉS SUR LES RÉSEAUX DE CHALEUR ET LES SOUS-STATIONS



**Heat production unit**

Biomass boiler, CHP, Waste incineration, etc.

Heat carrier Fluid

Pressurized water, steam

Distribution network

Two-pipes (supply / return)

Customers

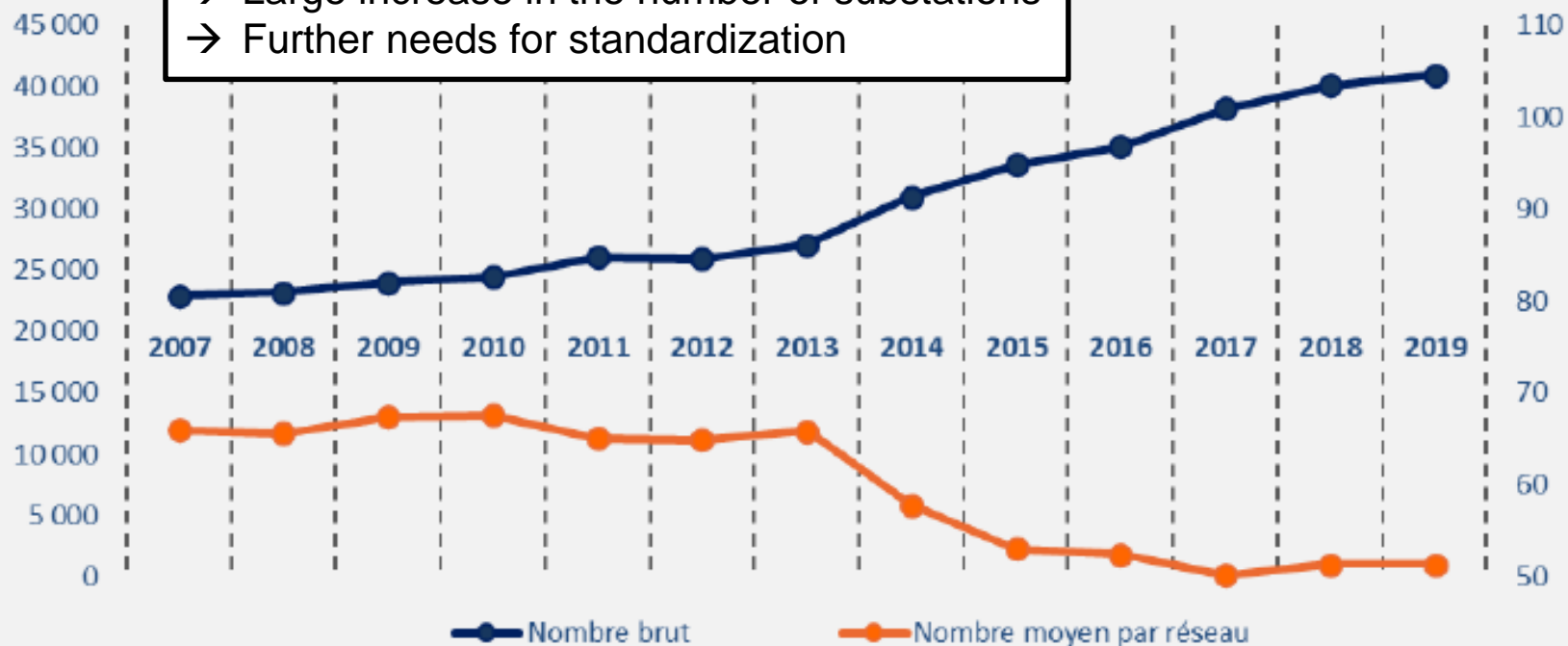
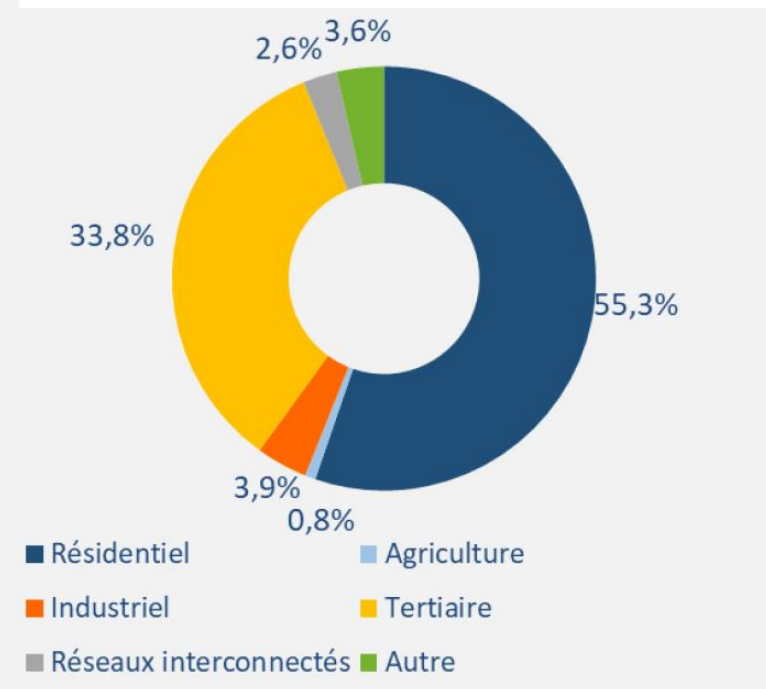
- DHW production
- Space heating
- (Industrial processes)

Sub-station

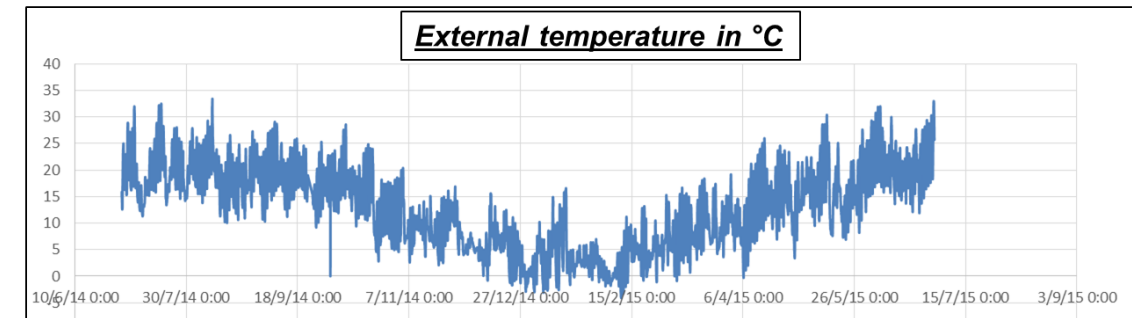
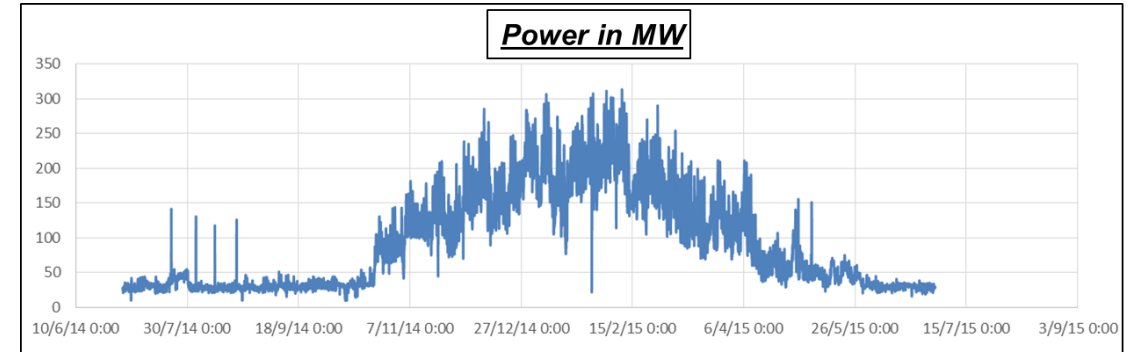
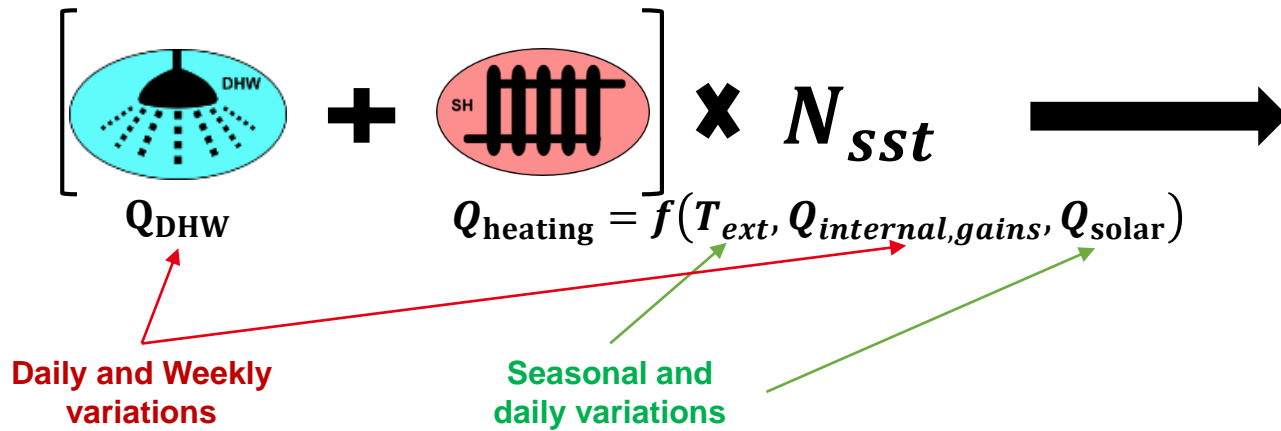
Where heat is delivered to the customer

Development of DHN

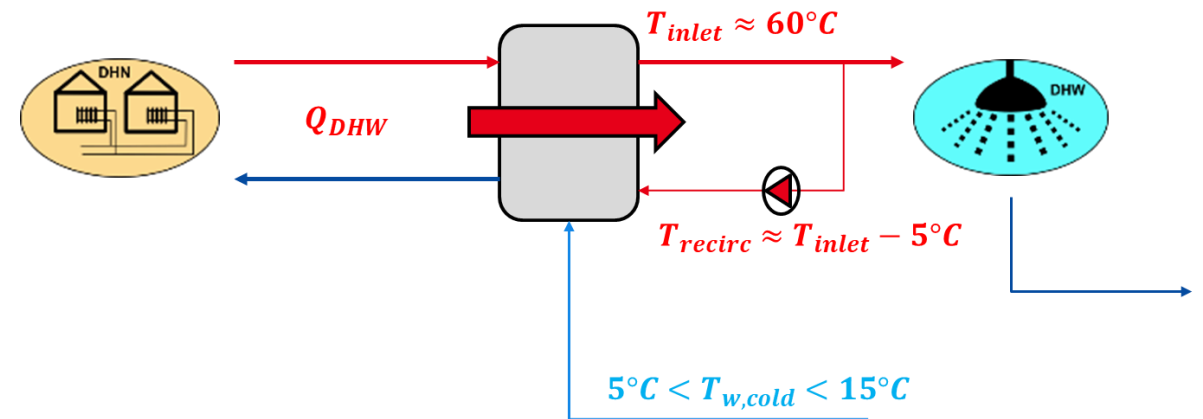
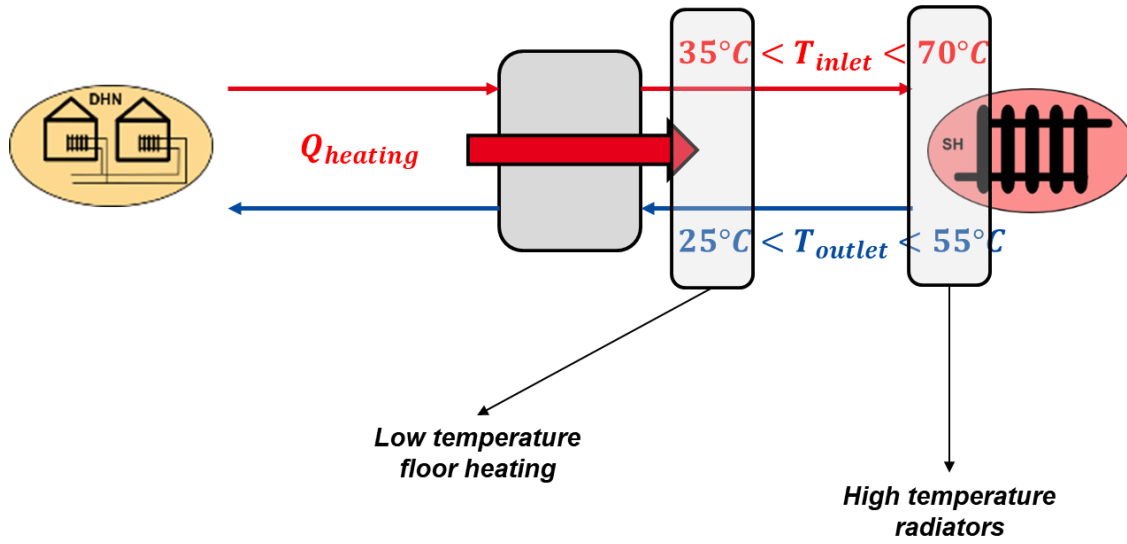
- Large increase in the number of substations
- Further needs for standardization

**Number of Substations****Delivery at customer**

Heat loads



Temperature Levels



RATED POWER

40kW



Flat substation
(DHW and SH separated)

300kW



~ 30 poorly insulated
housings

700kW



~ 70 poorly insulated
housings

10MW

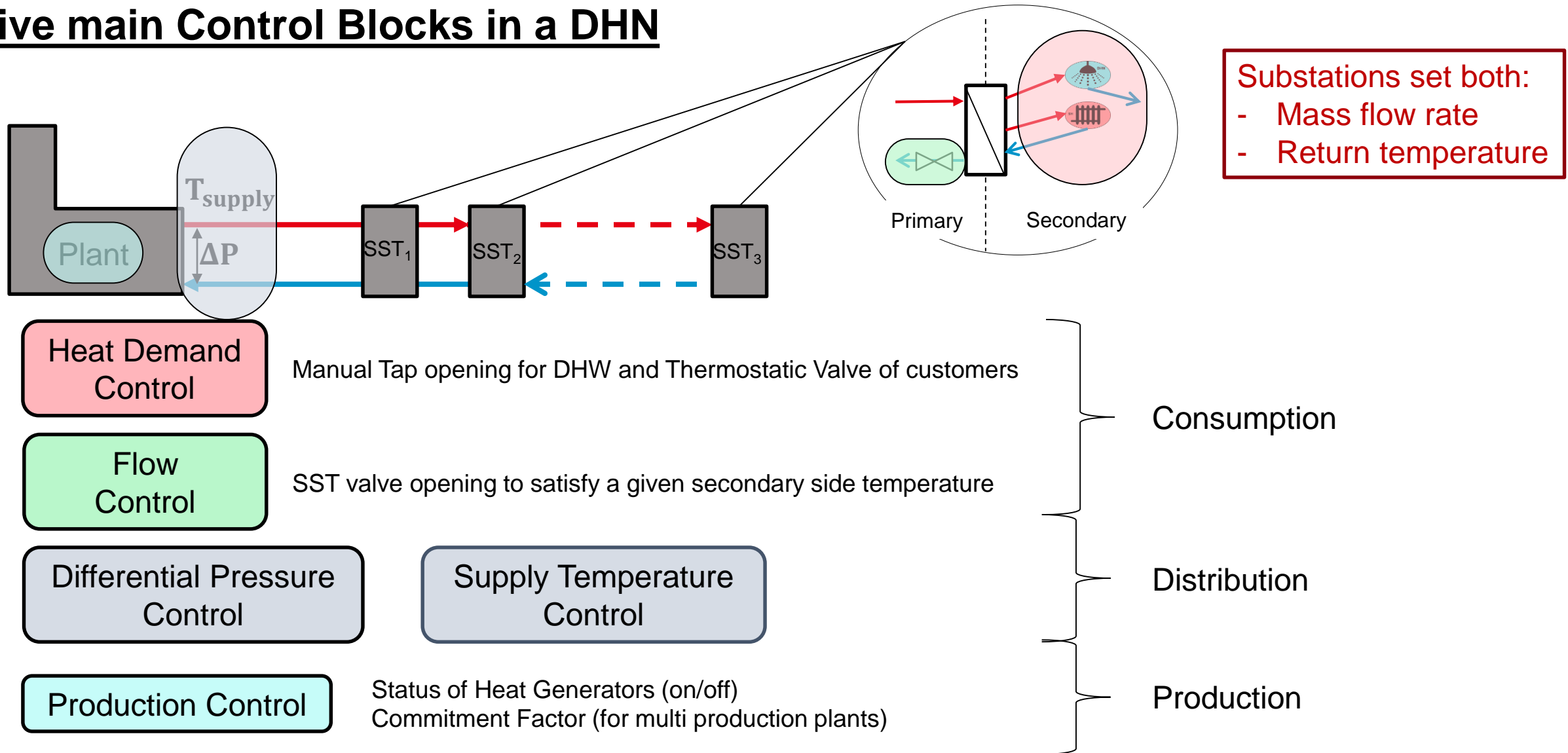


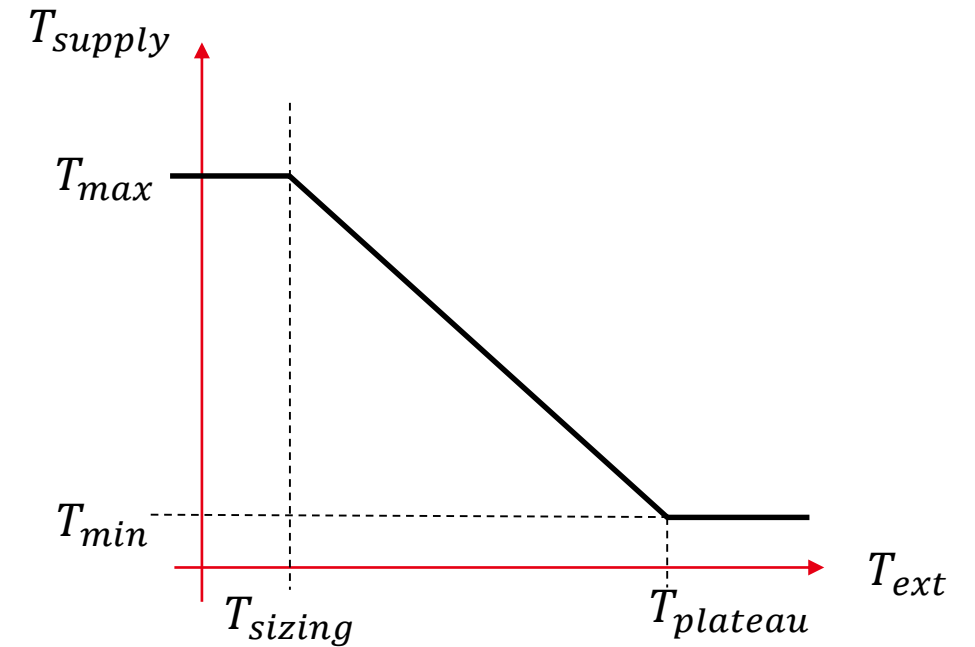
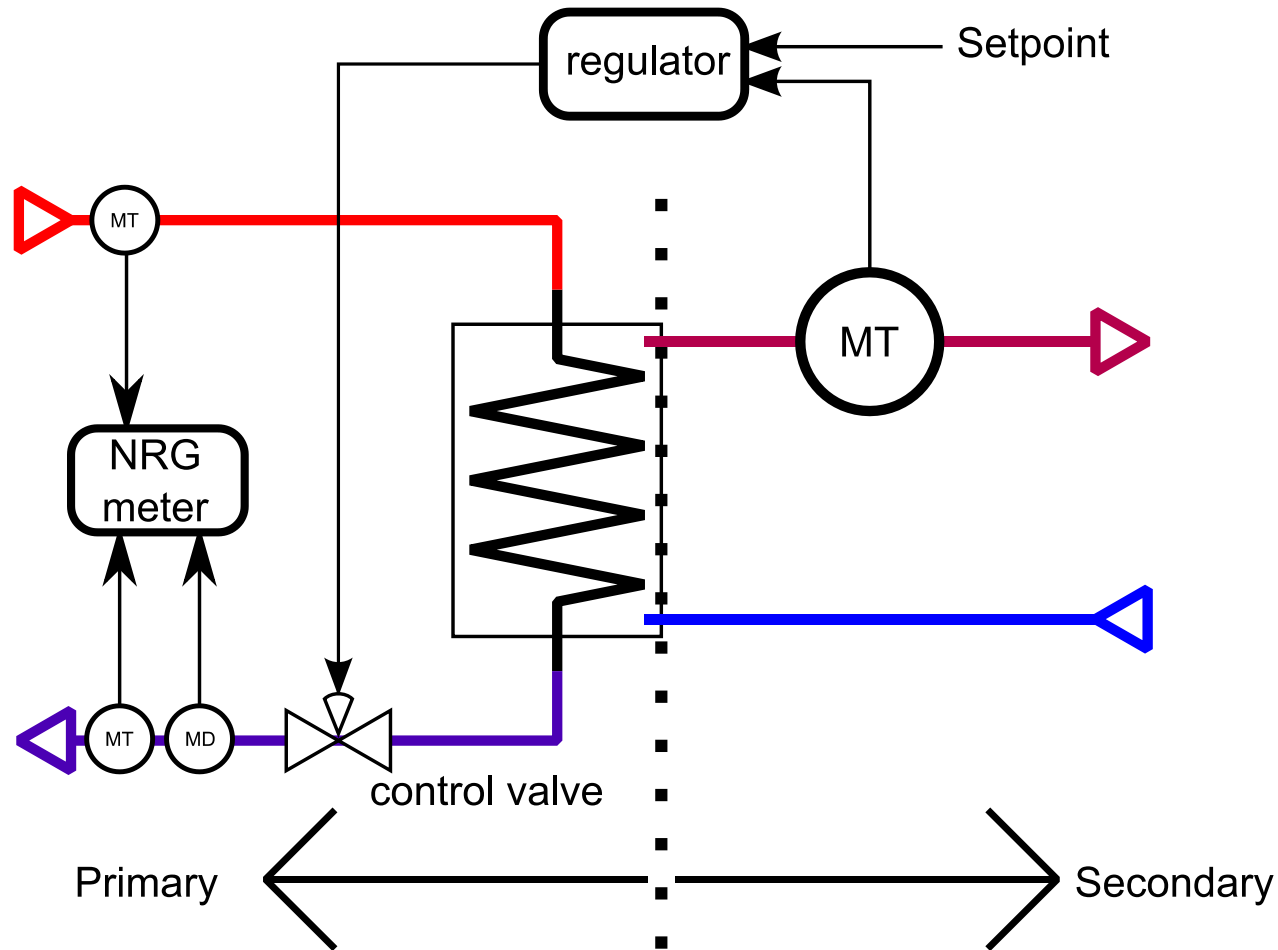
Area Substation between
HP and LP networks

Electrical Network Substation	Thermal Network Substation
Voltage Level Lowering	Temperature and Pressure Level Lowering
Significant High to Low Voltage difference	Small High to Low Temperature and Pressure difference
Located far from Buildings and serve a large area (to avoid risks)	Located close to the Building it is supplying (to reduce heat loss)
Transformers	Heat Exchangers and Valves
Fuses	Differential pressure control valve and flow limiters
Utility company ownership	Shared ownership (building owner and utility company)
Very standardized	Standardization still needed to further reduce costs

ARCHITECTURE ET CONTROLE

Five main Control Blocks in a DHN



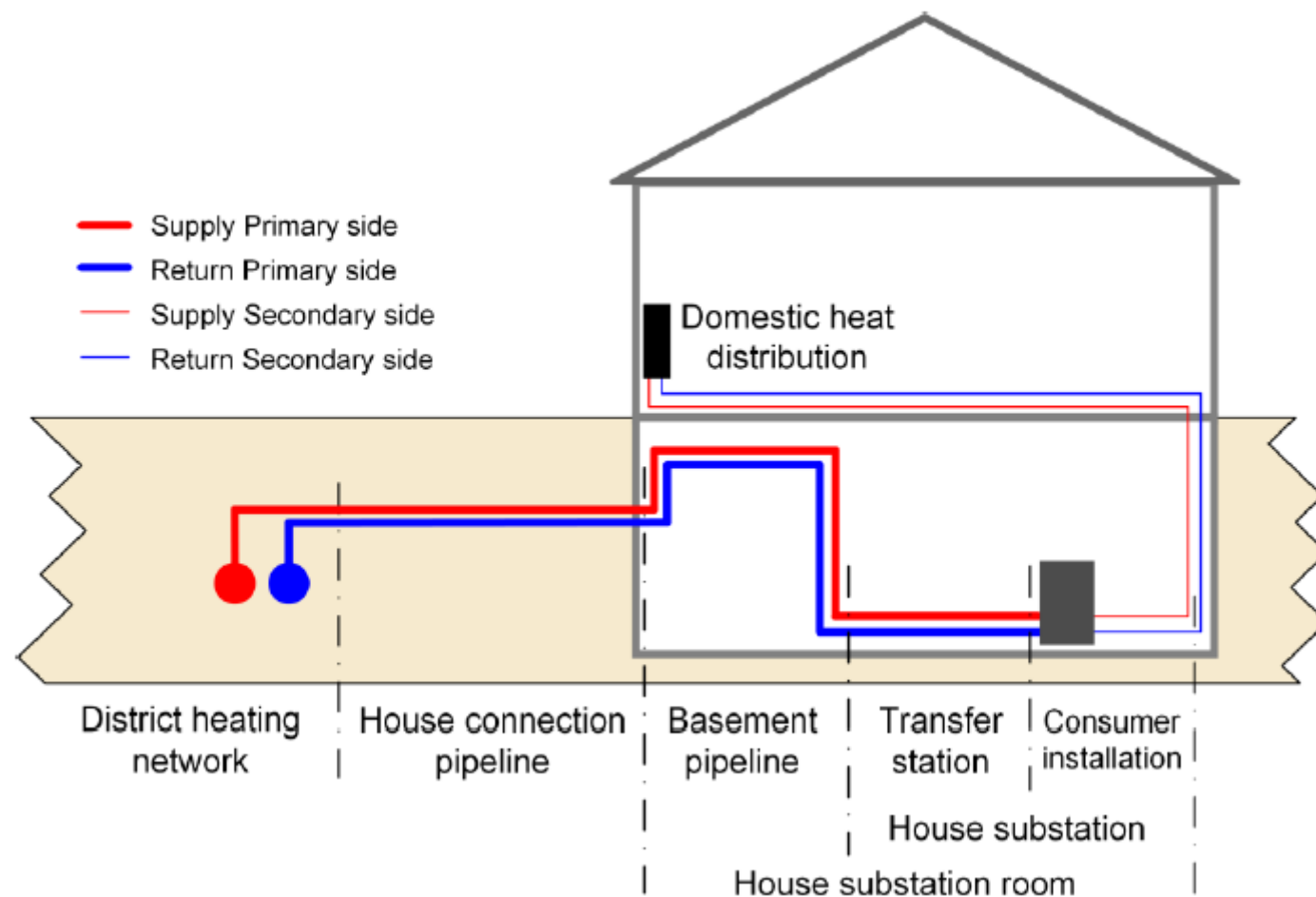
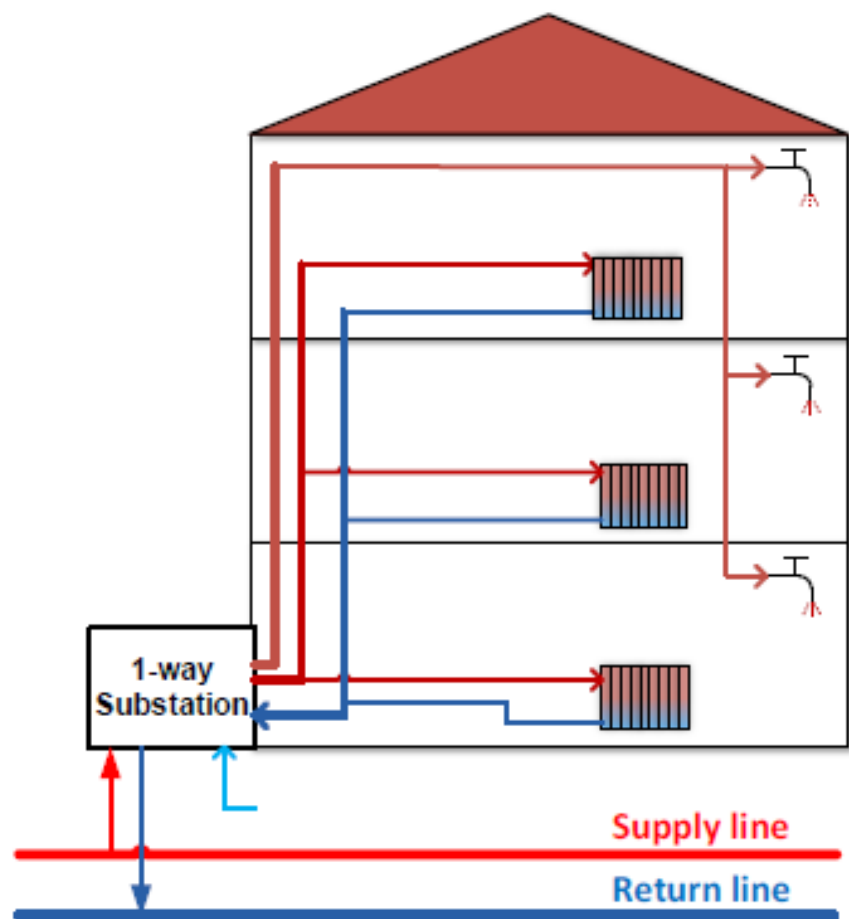


Optimal Operation

Reduce the return temperature

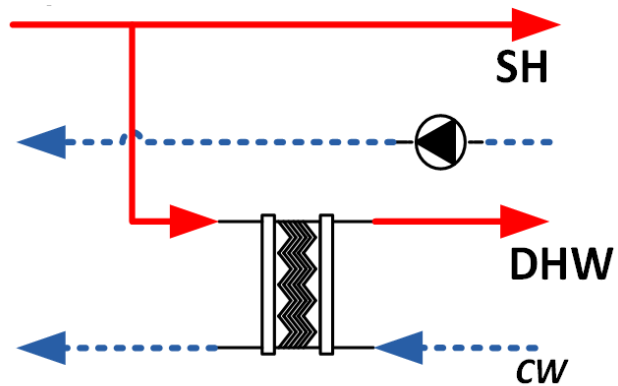
- Lower HL in return line
- Higher efficiency of the production units
- Lower mass flow rate in the network

Main layout for building substation



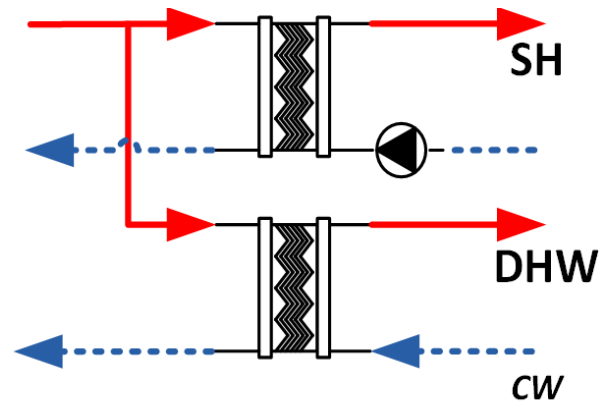
3 main layouts

Direct SH and Closed
DHW supply



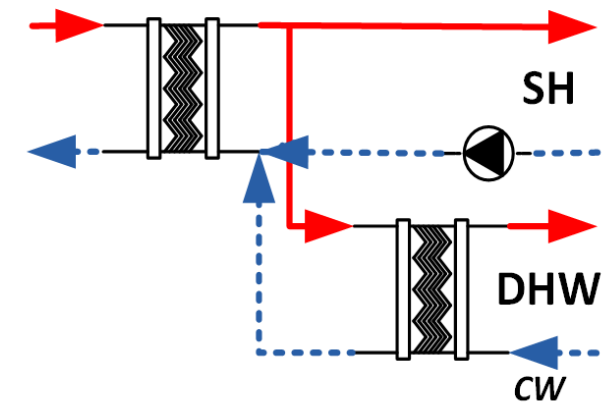
- + Low cost
- + No HEX pinch for SH
- Reference in Germany / Denmark

Indirect SH and Closed
DHW supply



- + Protects hydronic system (pressure surges, corrosion due to oxygen content)
- + Low pressure requirements for hydronic system
- + Reduced damage if leaks
- + Reduced noise propagation
- Reference in Sweden

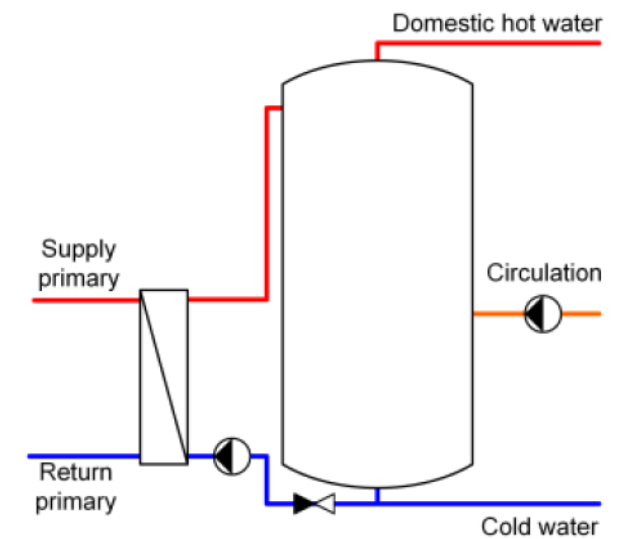
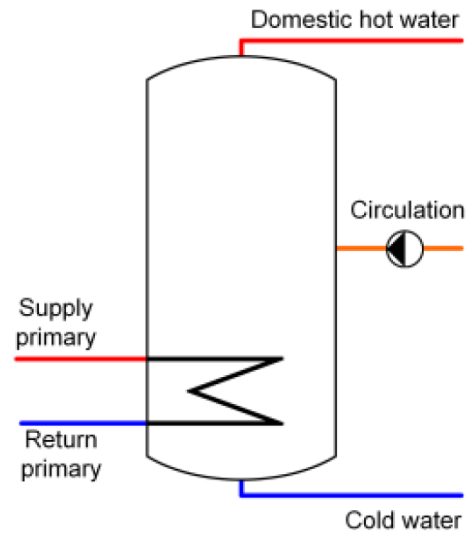
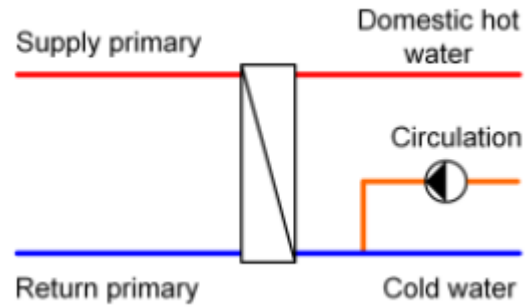
Intermediate SH circuit



- + Further protected DHW system against HEX leaks with DHN water
- Double HEX pinch for DHW
- SH circuit always higher temperature than DHW temperature
- Sometimes preferred in Germany

Other seldom layouts: No hydraulic separation / open hot water supply / double-walled DHW circuit separation

Type of DHW systems



Instantaneous DHW

- + Even out loads (asynchronous)
- + Few space required
- + No limit of energy for a draw-offs
- + Reduced legionella
- Demanding for the control system

$$T_{p,out} \sim 25 - 30^{\circ}\text{C}$$

Internal HEX Storage Tanks DHW

- + Better for small SH demand because no need to oversize service lines
- + Peak loads ensured by tank
- + Insensitive to lime scale
- Management of legionella
- Add heat losses (but small)

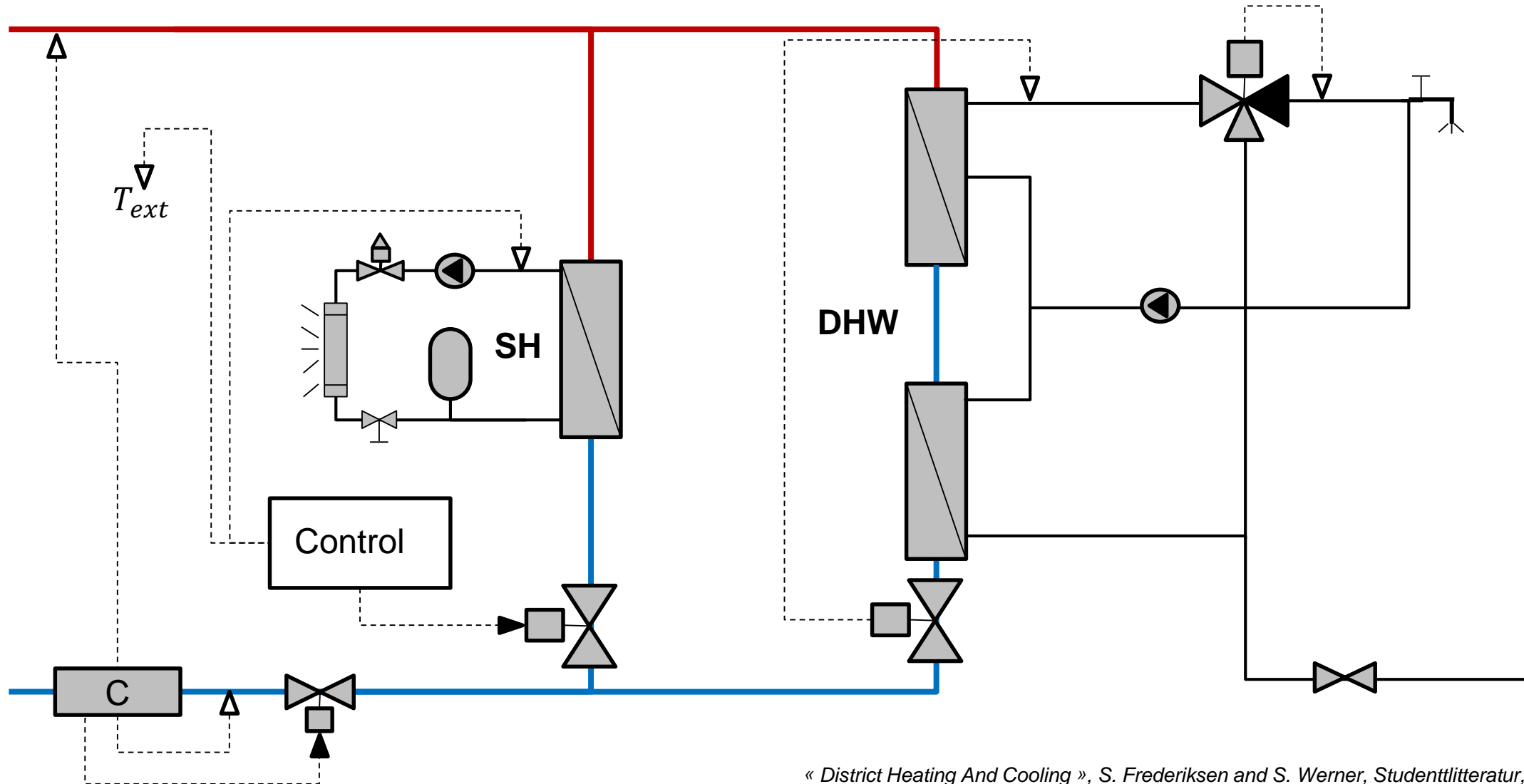
$$T_{p,out} \sim 45^{\circ}\text{C}$$

External HEX Storage Tanks DHW

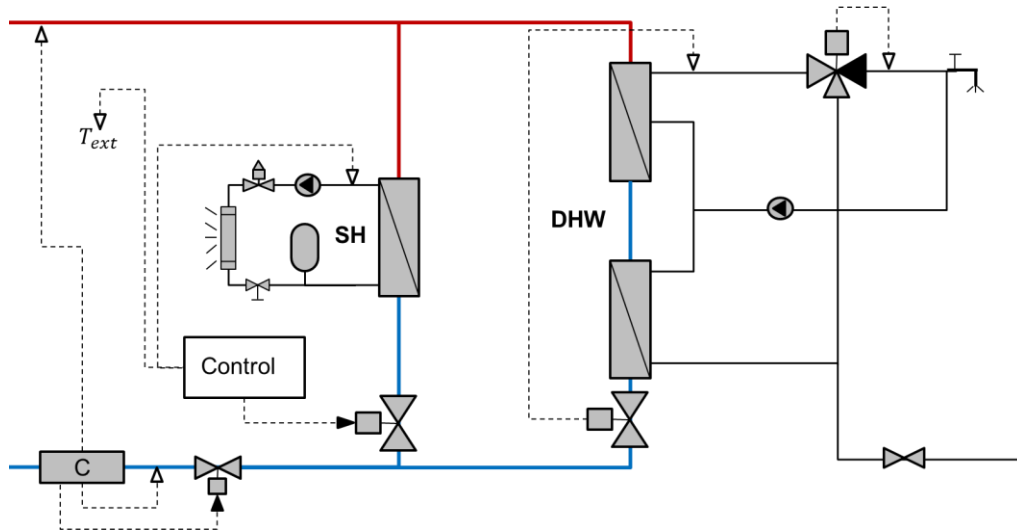
- + Better for small SH demand because no need to oversize service lines
- + Peak loads ensured by tank
- + Largest storage utilization
- Management of legionella
- Add heat losses (but small)

$$T_{p,out} \sim 30 - 35^{\circ}\text{C}$$

Detailed type of Indirect SH and Closed instantaneous cascading DHW supply



« District Heating And Cooling », S. Frederiksen and S. Werner, Studentlitteratur, Sweden, 2013



DHW loop

- Control of the valve on DHN side to satisfy a set point on the DHW loop based on legionella constraints
- Set point is generally higher than necessary and will be mixed in the 3way valve to avoid oscillations at the tap level
- Preheater / Postheater configuration to enhance DT because of recirculation sanitary loop
- Check valve on Cold Water Flow side

SH loop

- Control of the valve on DHN side to satisfy a set point on the SH loop based on external temperature measurement
- Control using self-regulating thermostatic valve
- Another valve for emitter isolation or hydraulic balancing
- Variable or Fixed speed circulation pump to maintain flow
- Expansion tank necessary to:
 - set the pressure in the loop
 - compensate for thermal expansion and contraction of heat carrier fluid

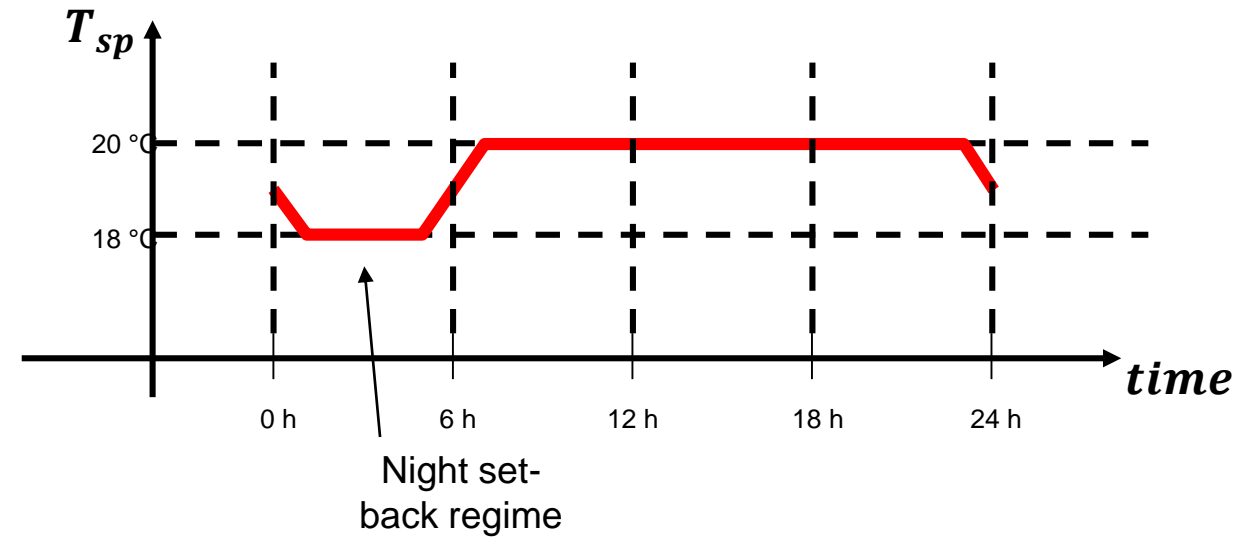
DHN loop

- Heat Meter for billing uses 2 temperature sensors and 1 flow meter
- A flow limiter can be used depending on contract with customer to limit energy to transfer and allow more favorable situations for far customers
- Return temperature limiter also exists

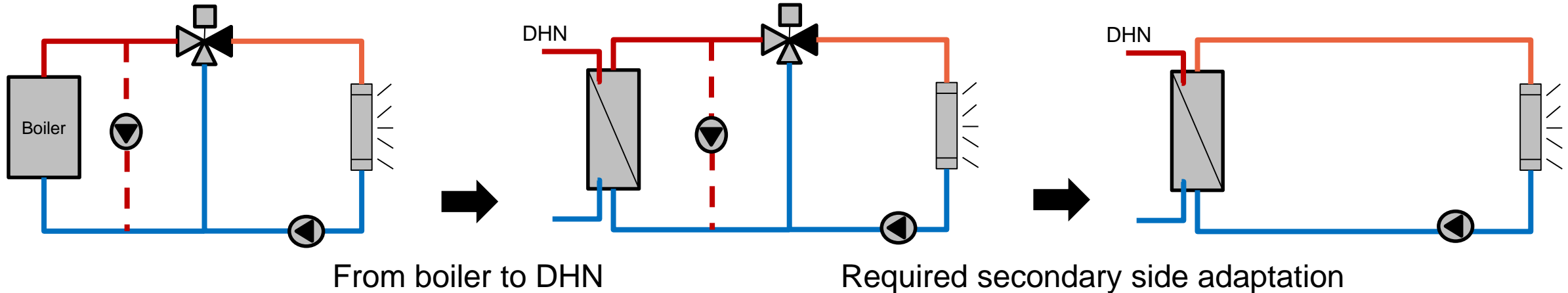
1) Night Setback

Save energy at night BUT
Generates high space heating loads in mornings

Flow rate increases before effect on return
temperature is observed



2) Transition from individual production system



Tube and Shell Heat Exchanger

- For high temperature and high pressure
- For large Substations (HP network to BP network)
- For old networks
- Problem of leaking after some years



Composed of :

- Tubes (high pressure fluid)
- One Shell and baffles for mixing
- Cross-flow heat exchange configuration

Straight-tube heat exchanger (two pass tube-side)

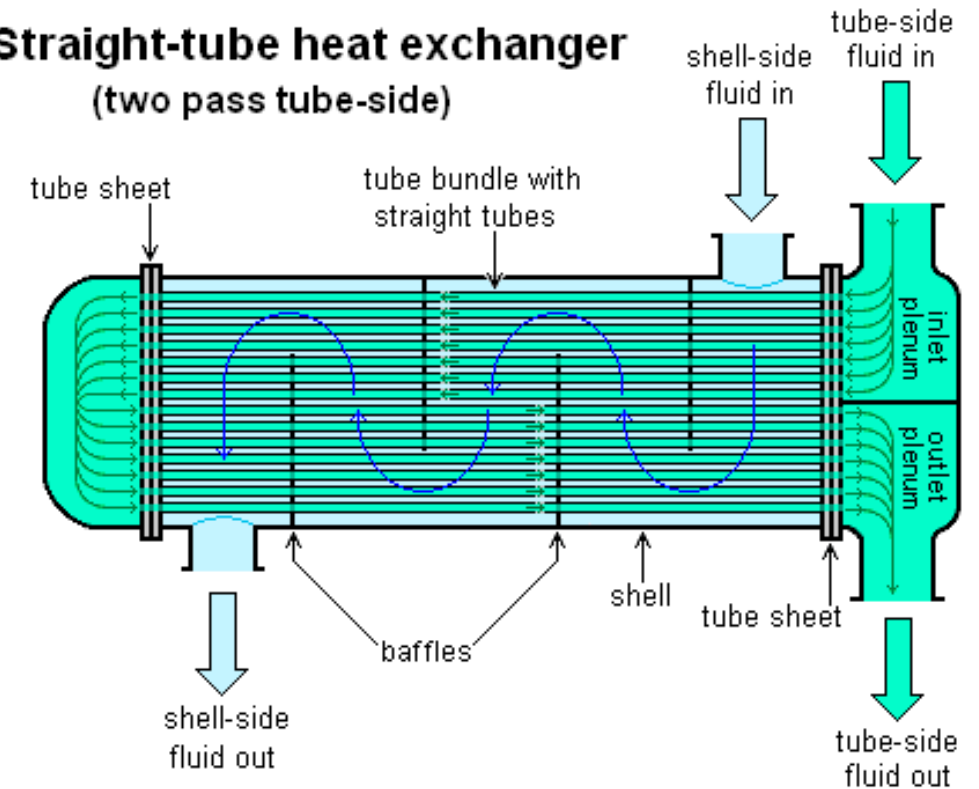
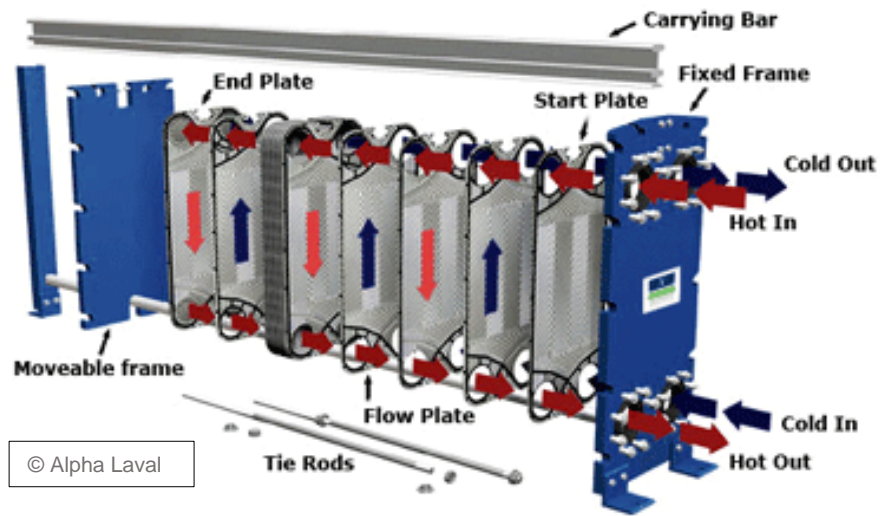


Plate Heat Exchanger

- Compact and high heat transfer performance
- Can be disassembled
- Number one solution in low temperature networks



Composed of :

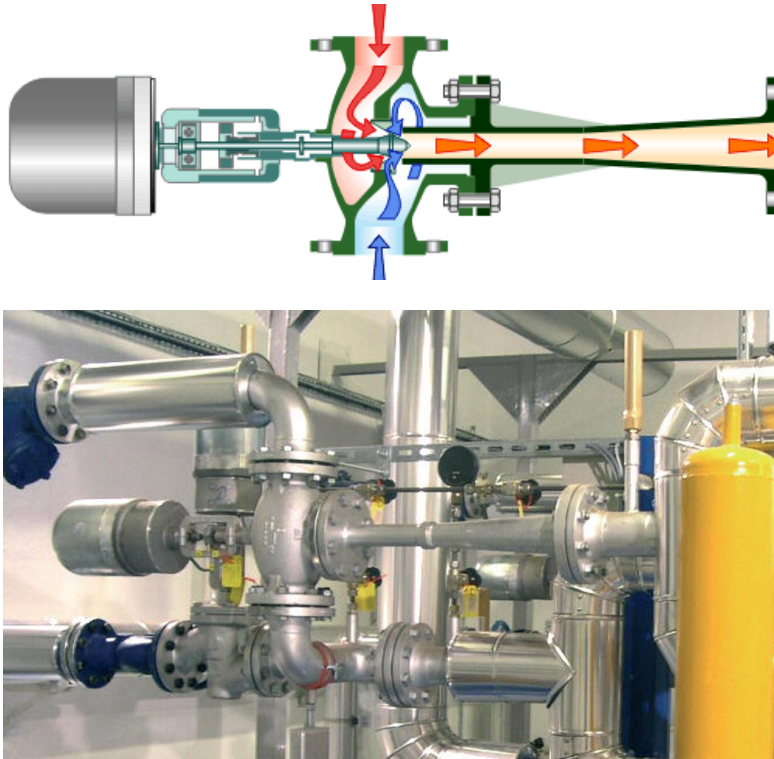
- Corrugated plates and gaskets
- Counter-flow heat exchange configuration
- « Hot » fluid flows down every even channel
- « Cold » fluid flows up every odd channel
- Gasketed or Brazed

Control Element

2way Valve



Hydro-Ejector



3way Valve



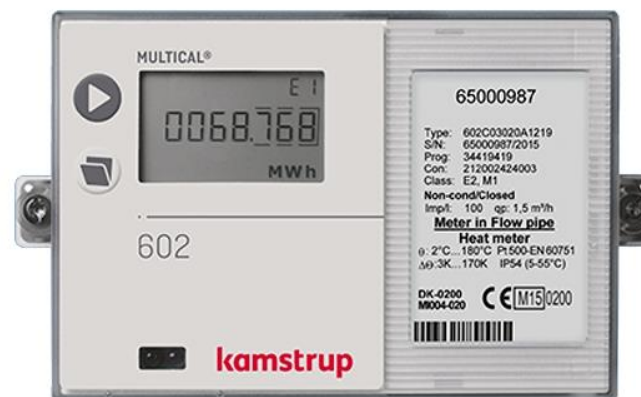
Instrumentations



Pressure



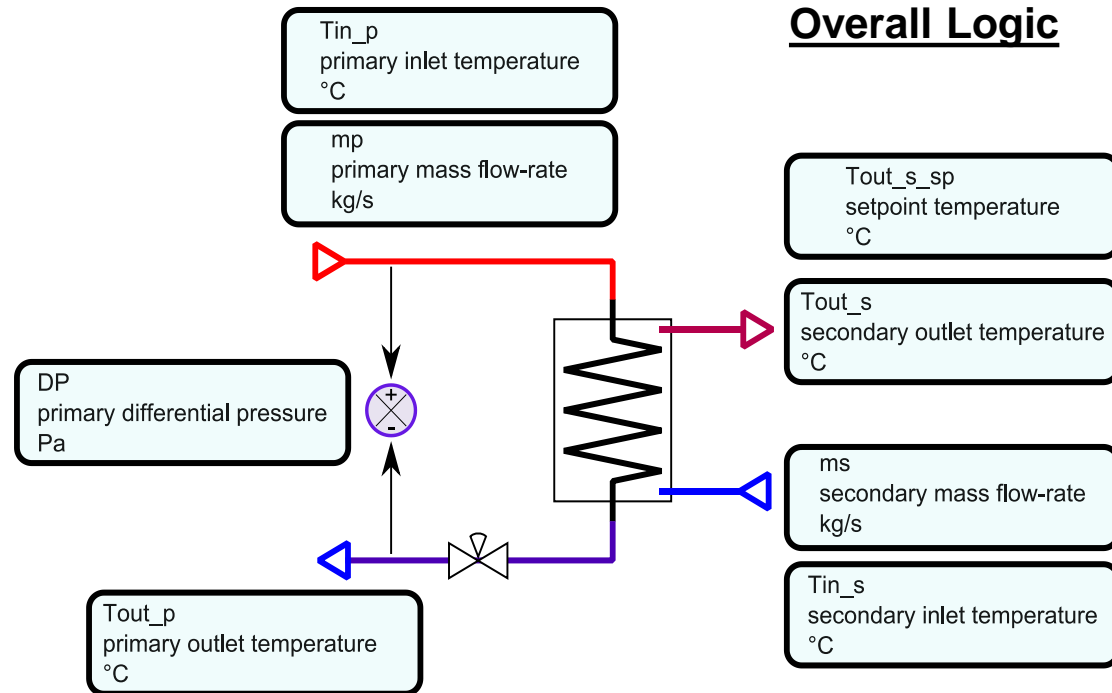
Temperature



Energy Meter



Flow Meter



Input Nominal Data

- Secondary Temperatures: $T_{in,s,nom}$ et $T_{out,s,nom}$
- Heat Load: $Q_{dem,nom}$
- Primary Inlet Temperature: $T_{in,p,nom}$
- Primary Differential Pressure: $\Delta P_{p,nom} = 1bar$
- Desired Pinch: $\Delta T_{pp,HEX}$

$$1) T_{out,p,nom} = T_{in,s,nom} + \Delta T_{pp,HEX}$$

$$2) \dot{m}_{p,nom} = \frac{Q_{dem,nom}}{c_p \cdot (T_{out,p,nom} - T_{in,p,nom})}$$

3) Fully Open Valve Authority:

$$\beta = \frac{\Delta P_v}{\Delta P_{p,nom}} \geq 0.5 \quad \text{with} \quad \Delta P_v = \left(\frac{\dot{m}_{p,nom} / \rho}{K_{v,s}} \right)^2$$

$$4) \dot{m}_{s,nom} = \frac{Q_{dem,nom}}{c_p \cdot (T_{out,s,nom} - T_{in,s,nom})}$$

5) Heat Exchanger Sizing

$$UA_{HEX} = \frac{Q_{dem,nom}}{DTLM_{HEX}}$$

$$\text{With} \quad DTLM_{HEX} = \frac{(T_{in,p,nom} - T_{out,s,nom}) - (T_{out,p,nom} - T_{in,s,nom})}{\ln \left(\frac{T_{in,p,nom} - T_{out,s,nom}}{T_{out,p,nom} - T_{in,s,nom}} \right)}$$

$$\text{And } \Delta P_{HEX} \leq (1 - \beta) \cdot \Delta P_{p,nom}$$

Heat Exchanger

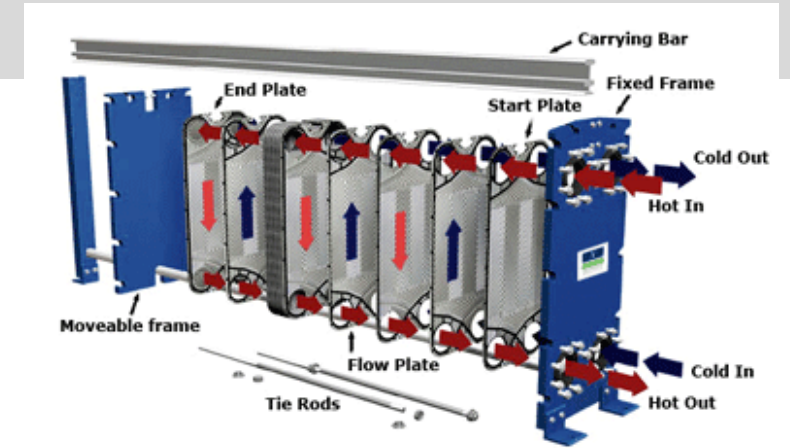
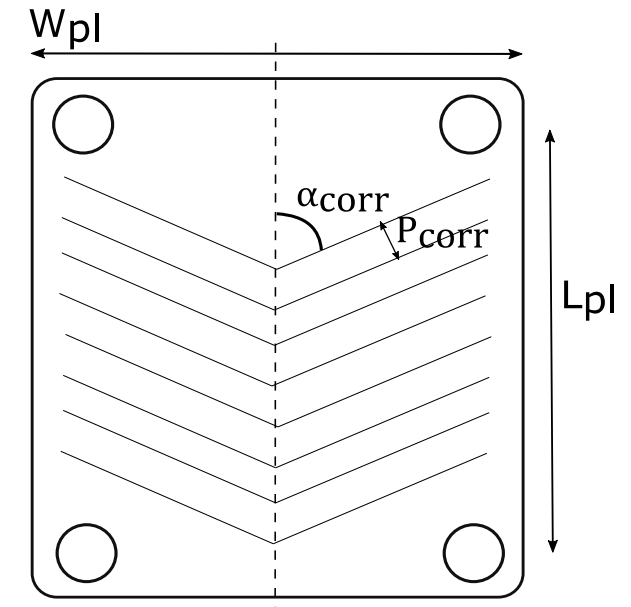
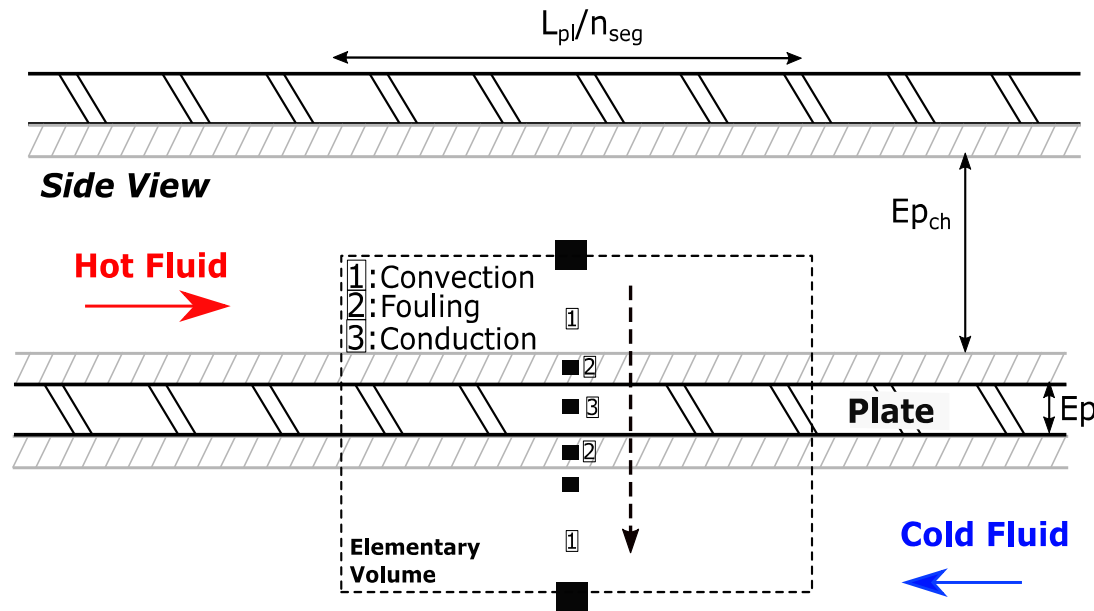
$$U = \left(\frac{1}{h_{conv,hot}} + \frac{1}{h_{fouling,hot}} + \frac{1}{h_{plate}} + \frac{1}{h_{fouling,cold}} + \frac{1}{h_{conv,cold}} \right)^{-1}$$

$\sim 5 \text{ kW} \cdot \text{m}^{-2} \cdot \text{K}^{-1}$ $\sim 45 \text{ kW} \cdot \text{m}^{-2} \cdot \text{K}^{-1}$ $\sim 10 \text{ kW} \cdot \text{m}^{-2} \cdot \text{K}^{-1}$

$\sim 20 - 200 \text{ kW} \cdot \text{m}^{-2} \cdot \text{K}^{-1}$

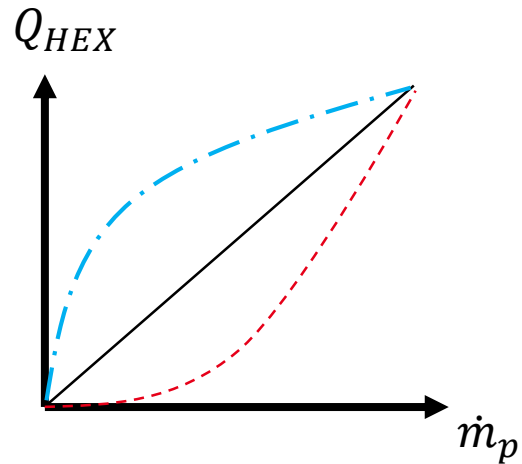
$$h_{conv} = k \cdot \frac{Nu}{d_h}$$

$$Nu = a \cdot Re^b \cdot Pr^{1/3}$$

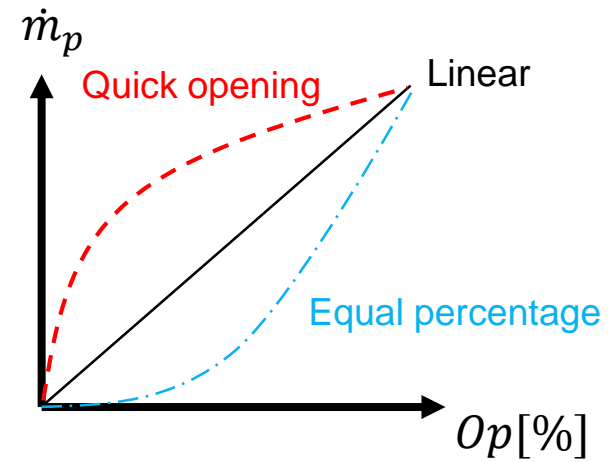


Valve

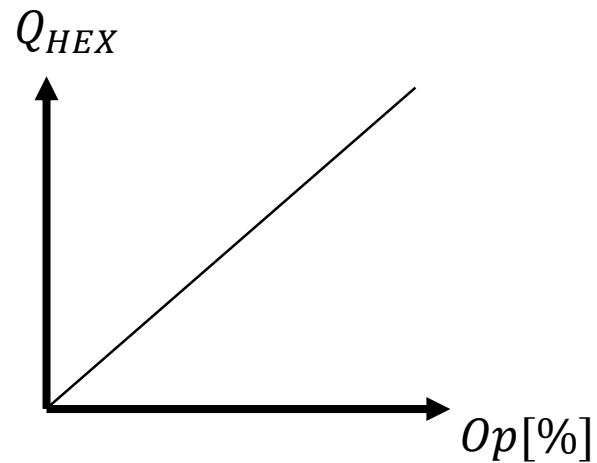
Heat Exchanger characteristics



Valve Characteristics



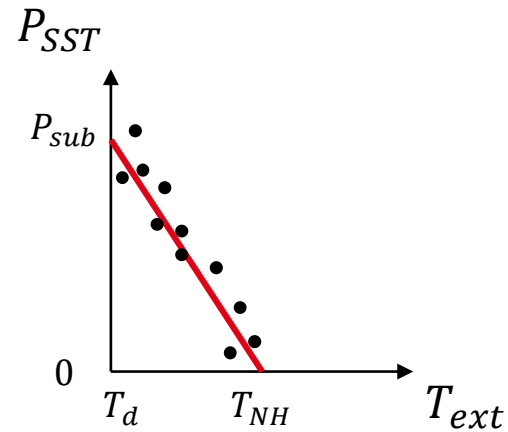
Substation characteristics



Always the same relative change in opening for equivalent relative demand variation

Data Analysis – Physical and Sociological Influences

Substation with
SH only



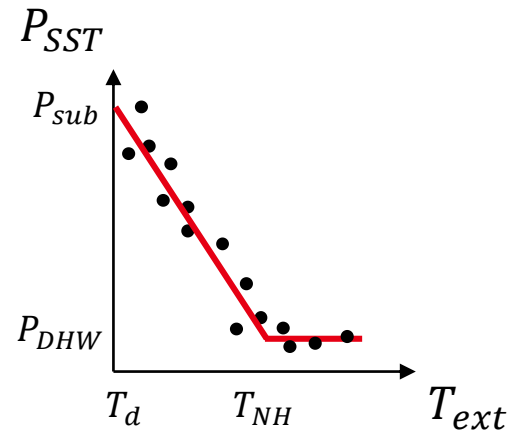
P_{sub} : Subscribed power

T_d : Design temperature

T_{NH} : Effective temperature

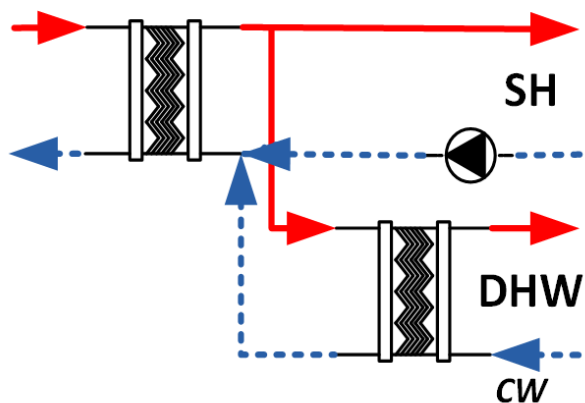
$$T_{NH} = T_{int} - \frac{Q_{internal\ gains} + Q_{solar}}{UA}$$

Substation with
SH and DHW

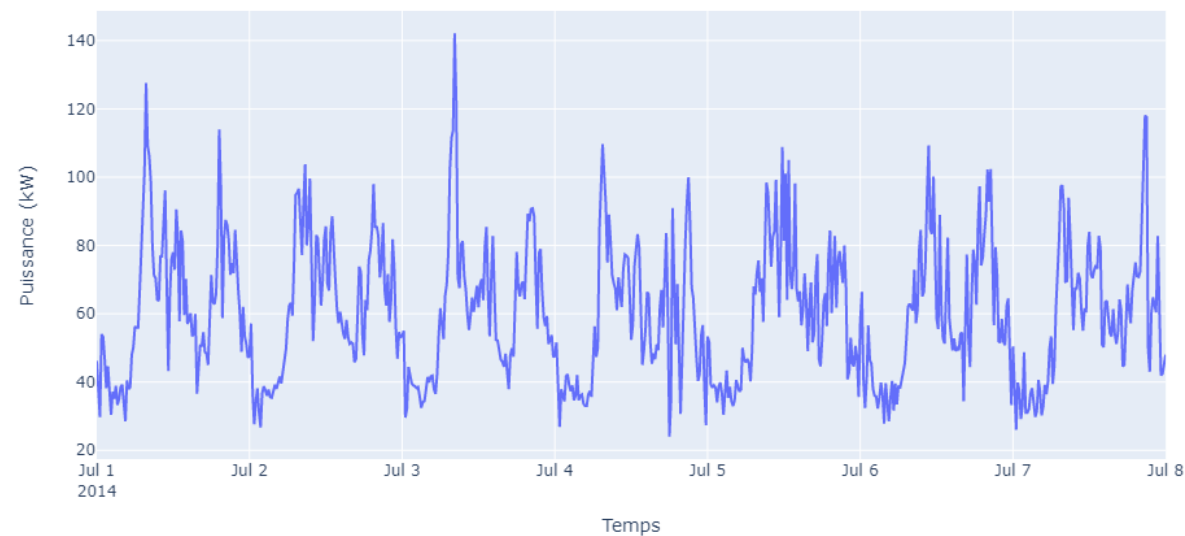
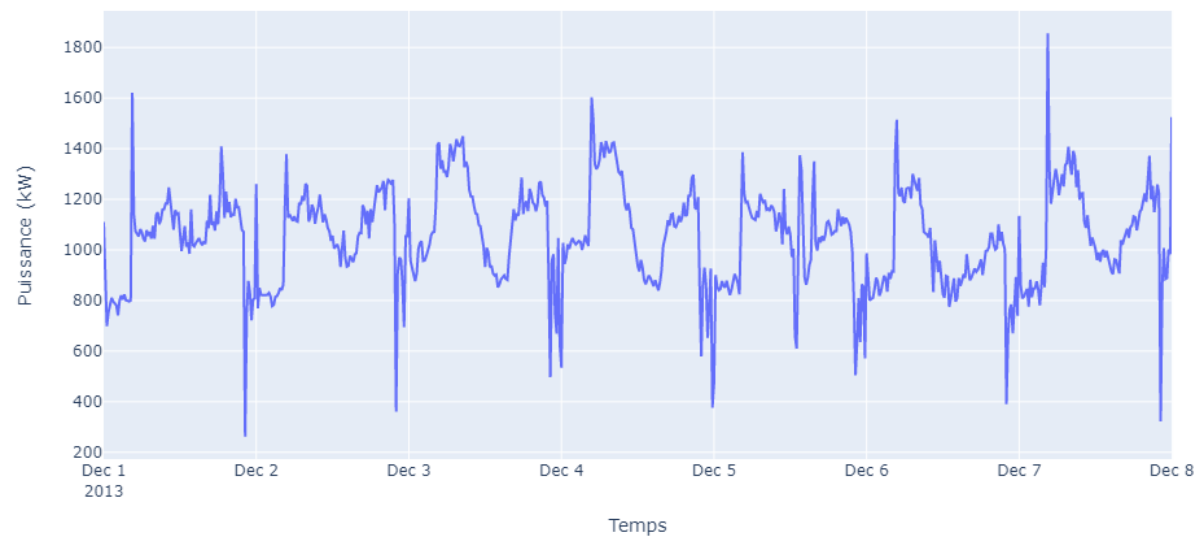


P_{DHW} : DHW mean power

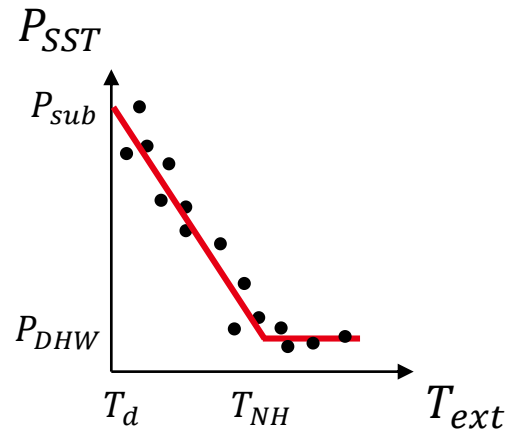
Data Analysis – Large Substation with SH and DHW demand



- Tubular HEX
- About 300 housings with radiators
- 20000m²
- No DHW storage



Data Analysis – Physical and Sociological Influences



$$P_{SST} = \begin{cases} P_{DHW,m} \cdot (1 + \delta P_{DHW,n,i}) & T_{ext} > T_{NH} \\ P_{DHW,m} \cdot (1 + \delta P_{DHW,i}) + a \cdot (T_{ext} + \delta T_{ext,i}) + b & T_{ext} < T_{NH} \end{cases}$$

$\delta P_{DHW,i}$ and $\delta T_{ext,i}$ are normed coefficients that can be reused as is for a similar type of customer

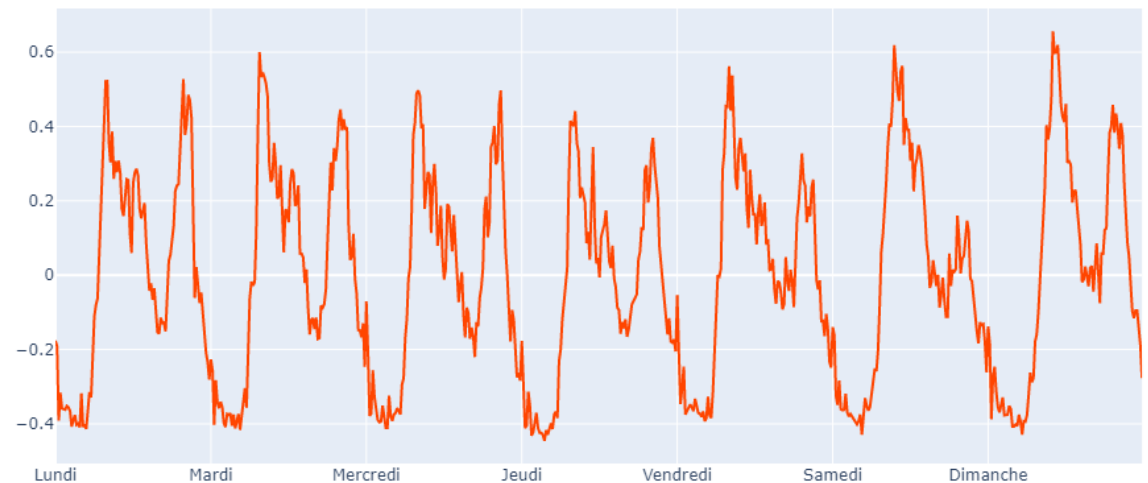
- Calculation during summer time of:
 - $P_{DHW,m}$: mean summer power
 - $\delta P_{DHW,n,i}$: normed weekly coefficient for sociological DHW needs
- During winter time, the DHW part is then removed and the data are fitted with a model $a \cdot (T_{ext}) + b \rightarrow$ **Physical contribution**
- The residuals are then calculated with $P_{SST} - P_{SST,fit}$ and are normalized by a to obtain residuals in °C
- These residuals represent the equivalent external temperature difference with respect to the current external temperature which would lead to the current demand
- These residuals are averaged for each time step of the week to obtain $\delta T_{ext,i} \rightarrow$ **Sociologic contribution**

SH sociologic contribution: $\delta T_{ext,i}$



- Night Setback
- Morning and Evening Peaks
- Maybe solar influence explains the peaks differences
- Less pronounced on sunday

DHW sociologic contribution: $\delta P_{DHWn,i}$



- Morning and Evening peaks

In 4th Generation District Heating Network, substations must face the following challenges:

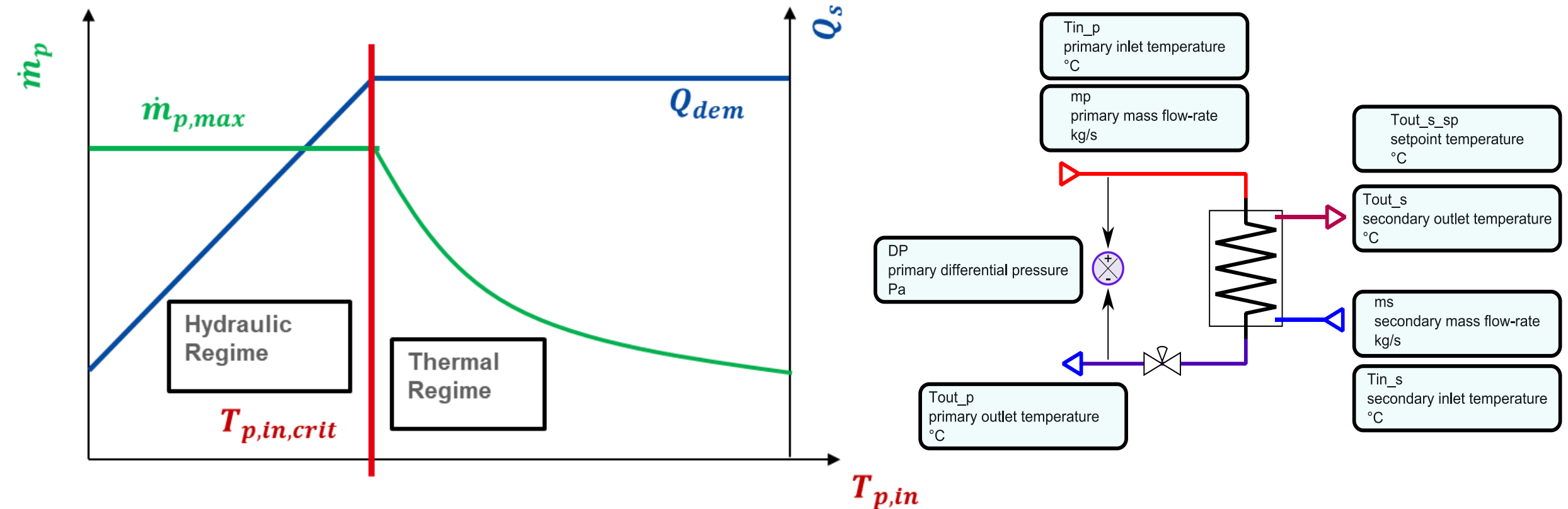
- Implement at fine sampling a digital monitoring
- Reduce the return temperature
- Limit loads on the production plants
- Reinject local surplus
- Reduced cost through standardization
- Combined District Heating and Cooling Substation including heat pumps

INNOVATION

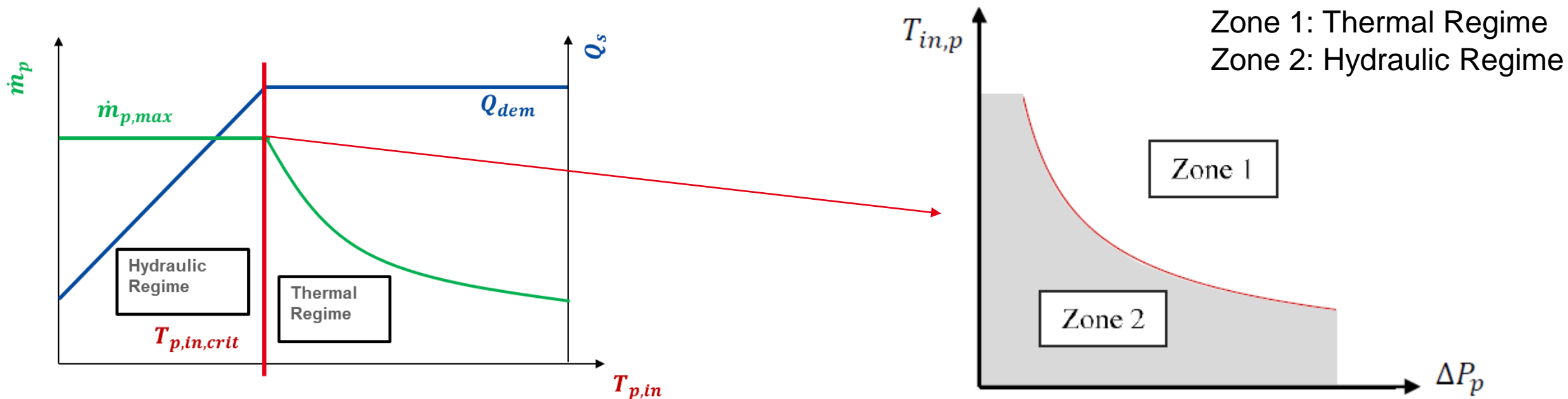
TOPIC 1:

Aim for the critical temperature at the entrance of the substation for a better supply temperature management in the District Heating Network

Limit loads on the production plants



For a given imposed differential pressure DP and a given heat demand on the secondary side, the critical temperature is the lowest possible primary inlet temperature that will satisfy the demand. In other words, it is the temperature that satisfies the demand when the valve is fully open.



Maximal primary flow rate

$$\dot{m}_{p,max} = \sqrt{\Delta P \left(\frac{\dot{m}_{HEX,nom}^2 \dot{m}_{v,nom}^2}{\Delta P_{HEX,nom} \dot{m}_{v,nom}^2 + \Delta P_{v,nom} \dot{m}_{HEX,nom}^2} \right)}$$

Secondary demanded flow rate

$$\dot{m}_{s,dem} = \frac{Q_{dem}}{cp(T_{s,out,set} - T_{s,in})}$$

Heat Exchanger performance

$$UA_{crit} = UA_{HEX,nom} \frac{\dot{m}_{p,nom,HEX}^{-q} + \dot{m}_{s,nom,HEX}^{-q}}{\dot{m}_{p,max}^{-q} + \dot{m}_{s,dem}^{-q}}$$

Primary critical temperature

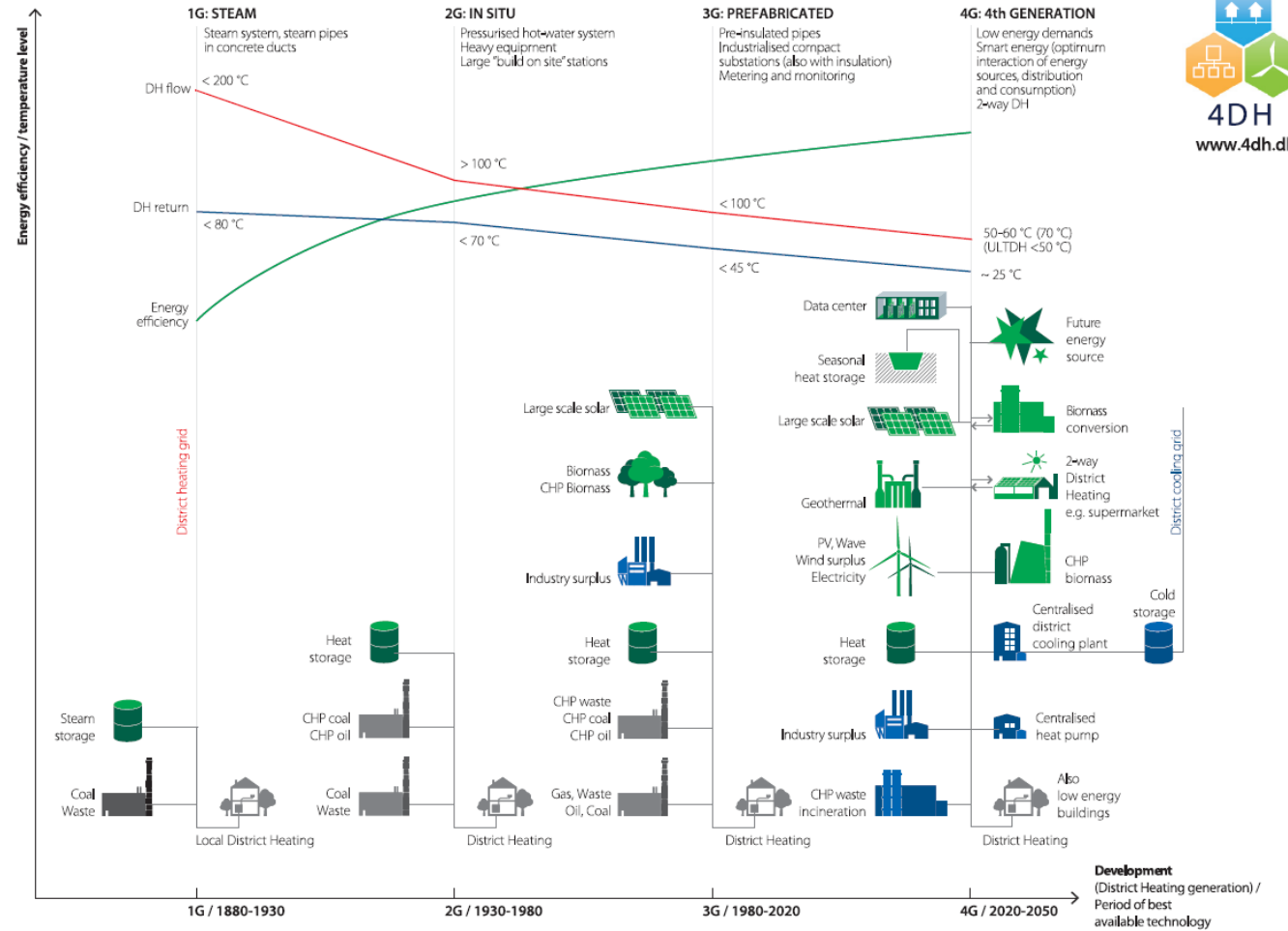
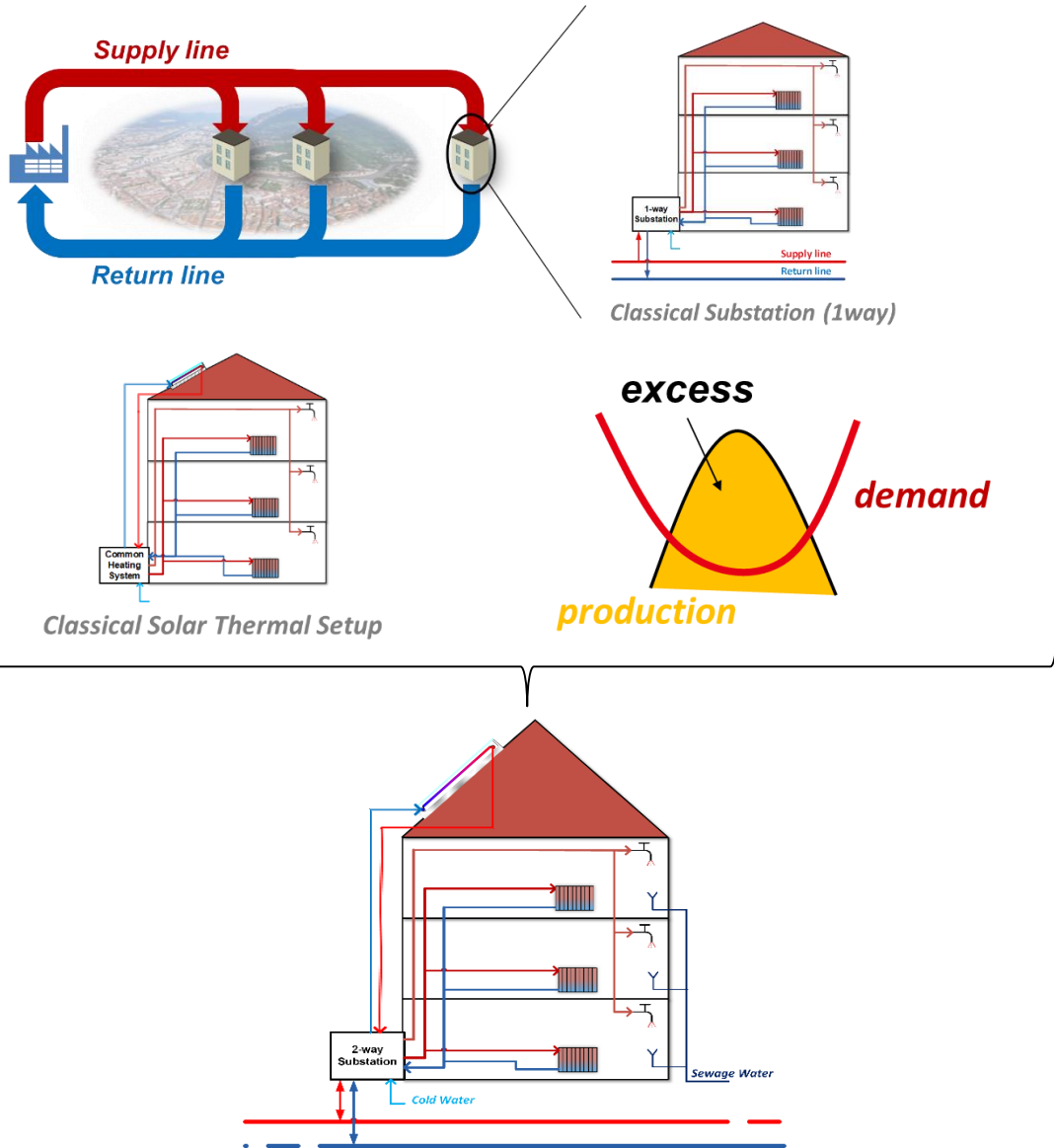
$$T_{p,in,crit} = T_{s,in} + \frac{Q_{dem}}{\dot{m}_{p,max} cp} \left[\frac{1 - \frac{\dot{m}_{p,max}}{\dot{m}_{s,dem}} \exp(A_c)}{1 - \exp(A_c)} \right]$$

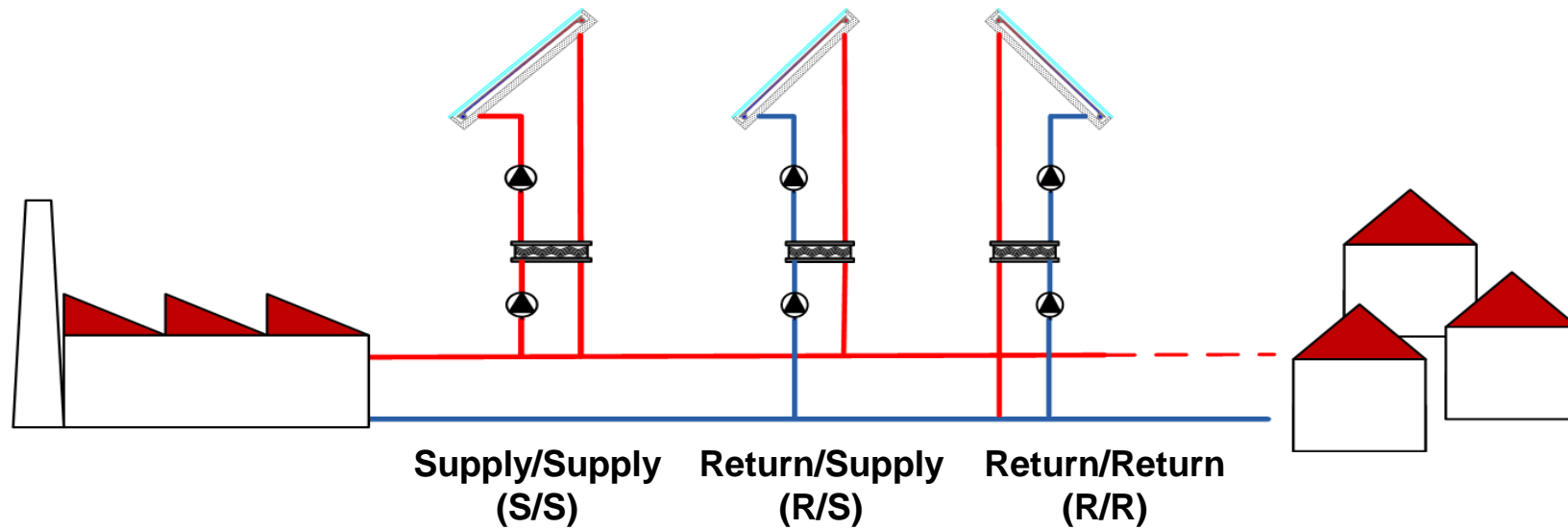
$$\text{With } A_c = - \frac{UA_{crit}}{cp \dot{m}_{s,dem}} \left[\frac{\dot{m}_{s,dem}}{\dot{m}_{p,max}} - 1 \right]$$

TOPIC 2:

Prosumer substation

Reinject local surplus





G. Lennermo et al., "Control of decentralised solar district heating", *Solar Energy*, Volume 179, 2019

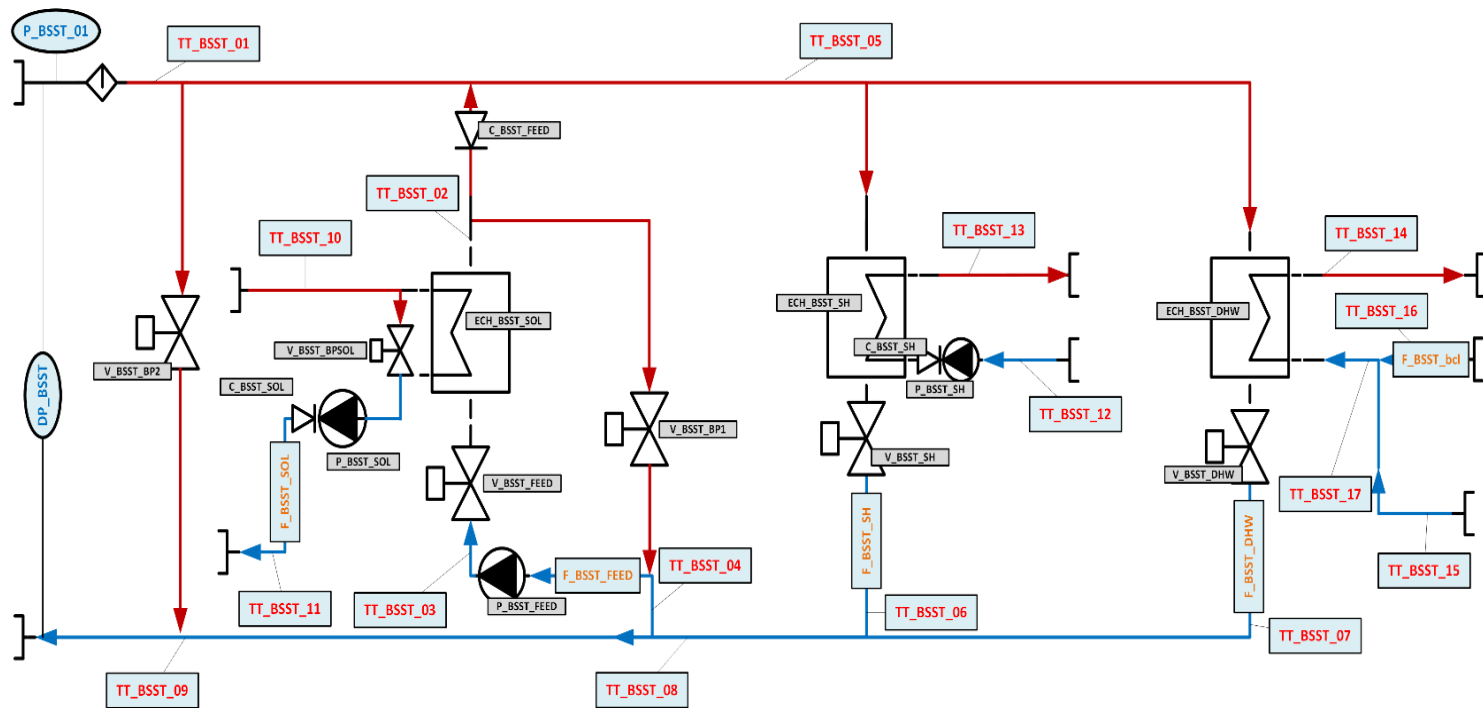
TYPE	ADVANTAGES	DISADVANTAGES	REMARKS
Supply/Supply (S/S)	<ul style="list-style-type: none"> No influence on return line 	<ul style="list-style-type: none"> Increase supply line temperature Lowest solar field efficiency Dependent on local flow rate Requires a third pipe Temperature Cycling → Pipe Fatigue 	<ul style="list-style-type: none"> Generally never used
Return/Return (R/R)	<ul style="list-style-type: none"> Highest solar field efficiency 	<ul style="list-style-type: none"> Increase return line temperature Lowest efficiency of centralized generators Dependent on local flow rate Requires a third pipe Temperature Cycling → Pipe Fatigue 	<ul style="list-style-type: none"> Seldom used Generally in combination with R/S
Return/Supply (R/S)	<ul style="list-style-type: none"> No influence on return line Use of existing service line Do not contribute to pipe fatigue 	<ul style="list-style-type: none"> High feed-in pump consumption Challenging control Feed-in temperature set by network 	<ul style="list-style-type: none"> Preferred solution



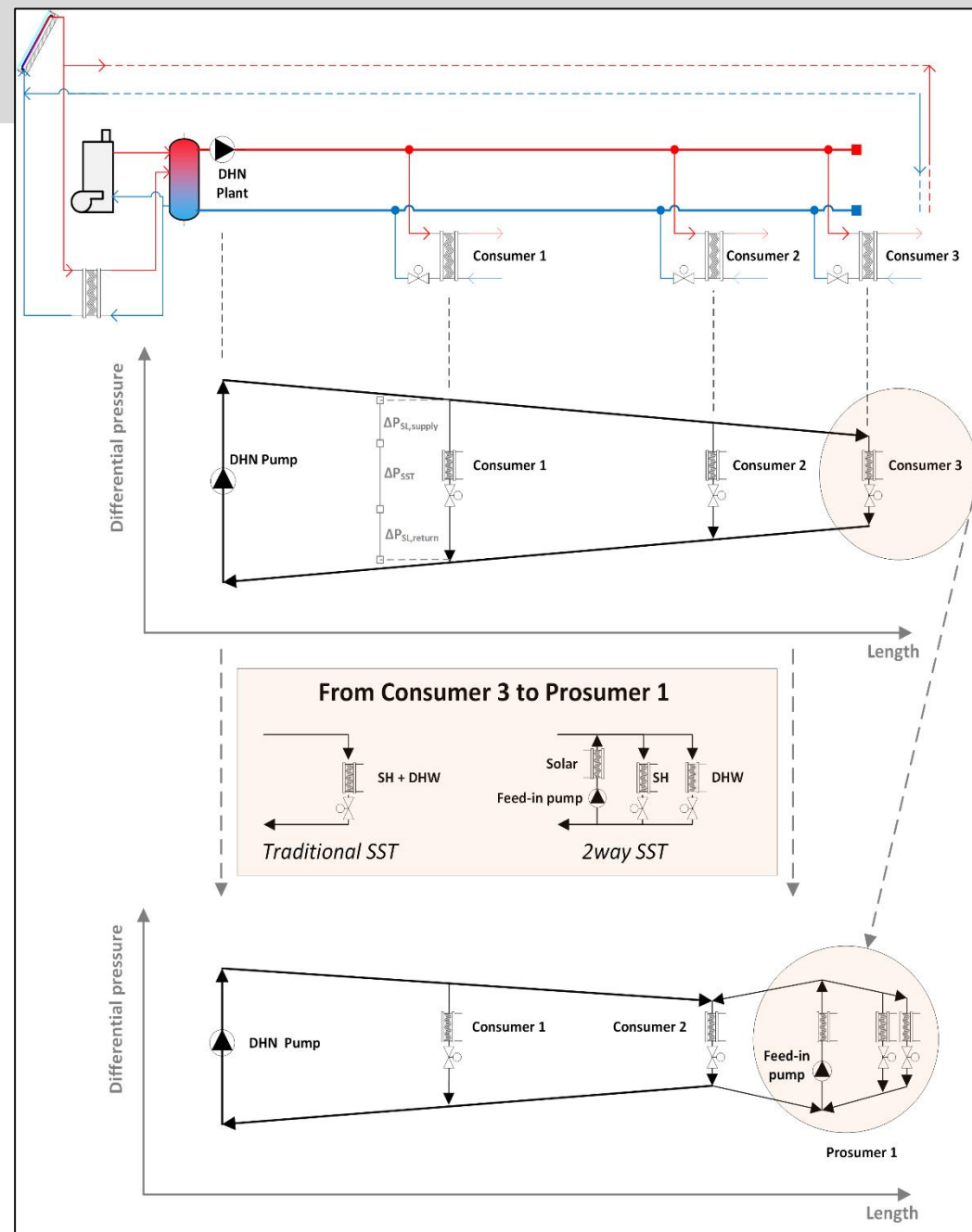
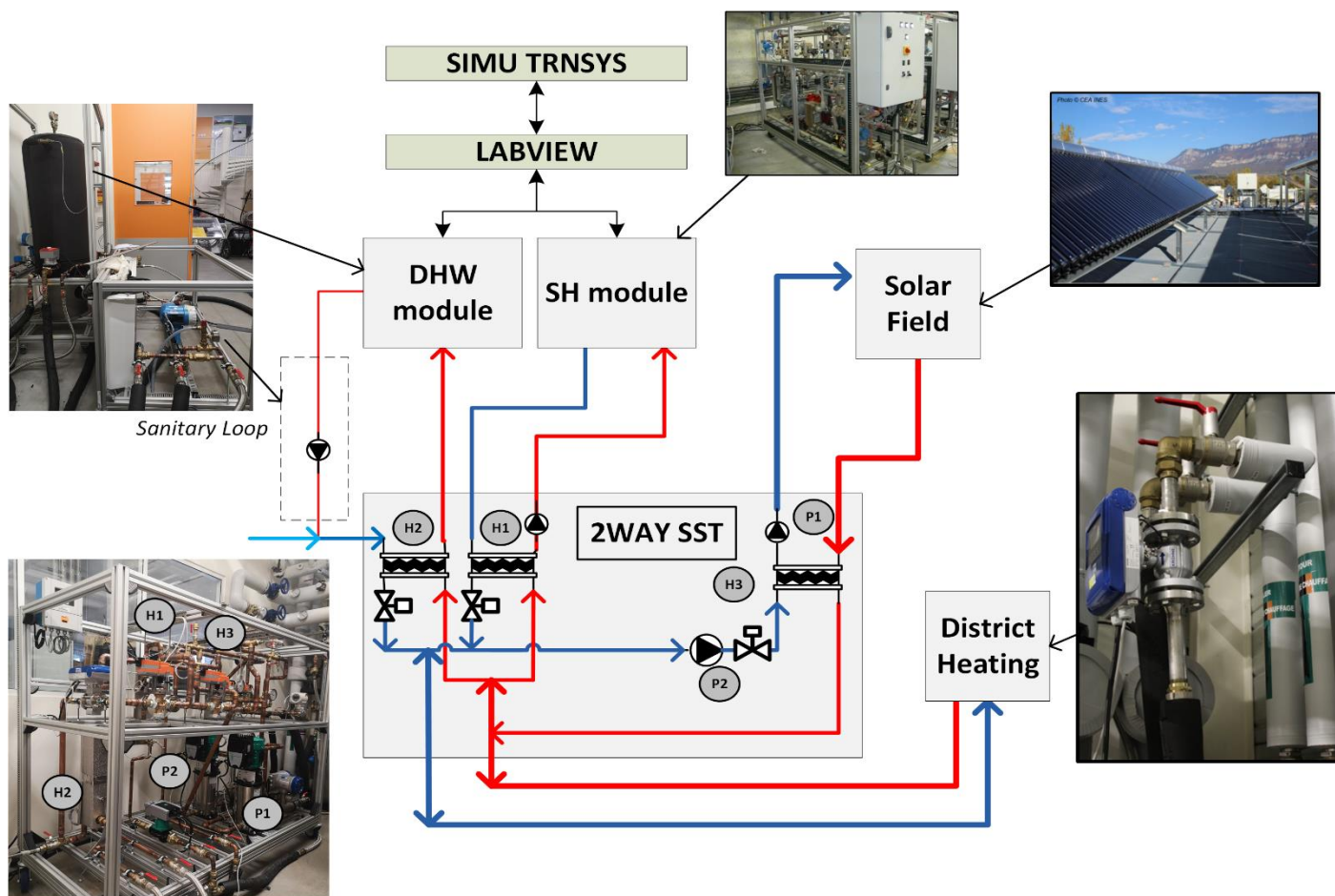
THERMOSS



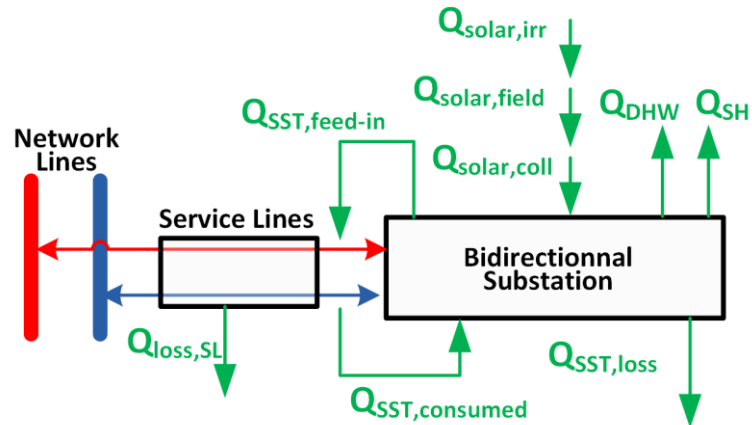
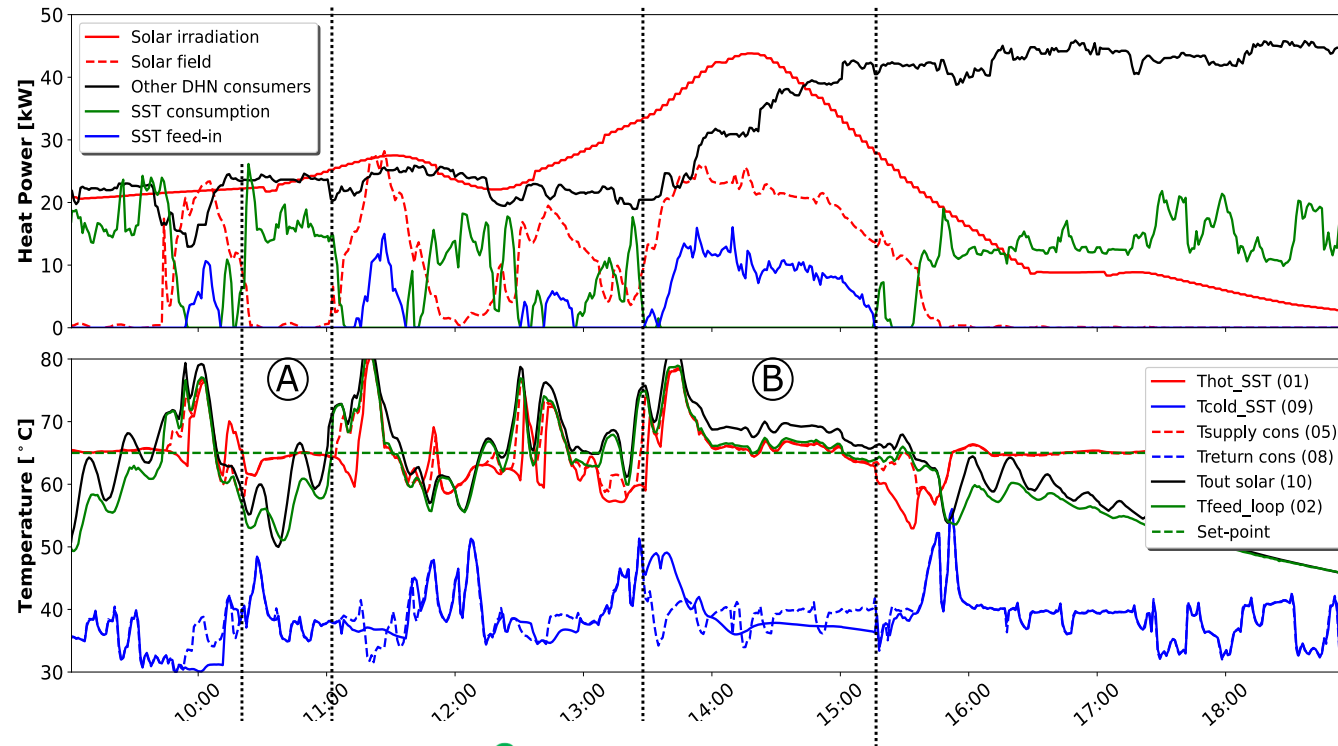
Thermoss Project
H2020 (2017 - 2020)



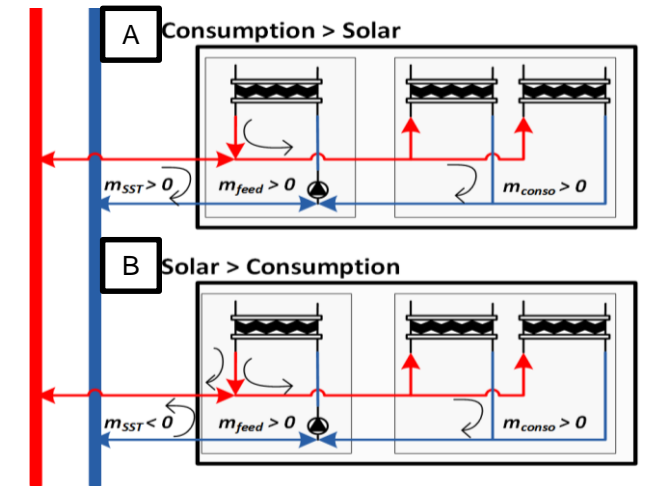
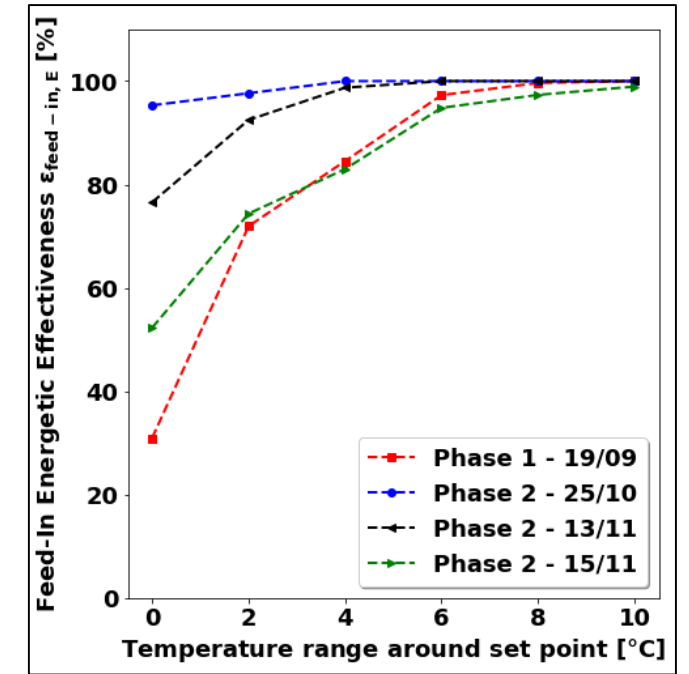
Prosumer substation = Feed-In + Consumer Substation



$$\varepsilon_{\text{feed-in},E,i} = \frac{\sum P_{\text{feed},in} \cdot \Delta t \big|_{F_{BSST_DHN} < 0 \text{ \& } TT01 > T_{sp}, TT01 - 2K}}{\sum P_{\text{feed},in} \cdot \Delta t \big|_{F_{BSST_DHN} < 0}}$$



$$SF_{\text{tot}} = \frac{E_{\text{SST,feed-in}} + E_{\text{SH}} + E_{\text{DHW}} - E_{\text{SST,consumed}}}{E_{\text{SH}} + E_{\text{DHW}}} = 25.5\%$$



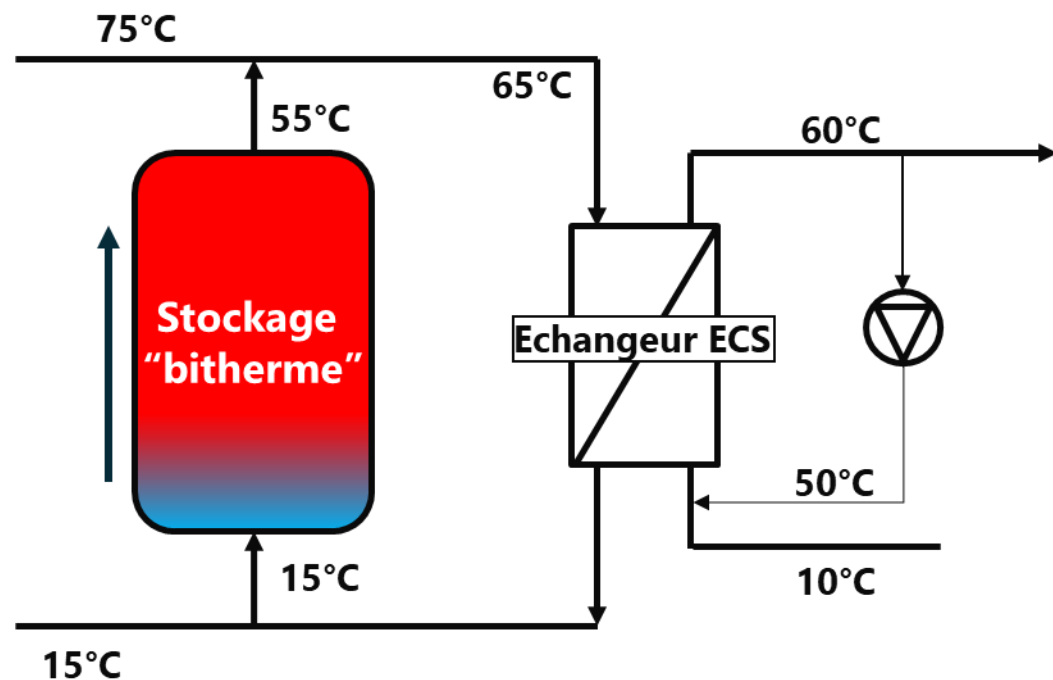
TOPIC 3:

Innovative design with primary storage

Limit loads on the production plants

Reduce the return temperature

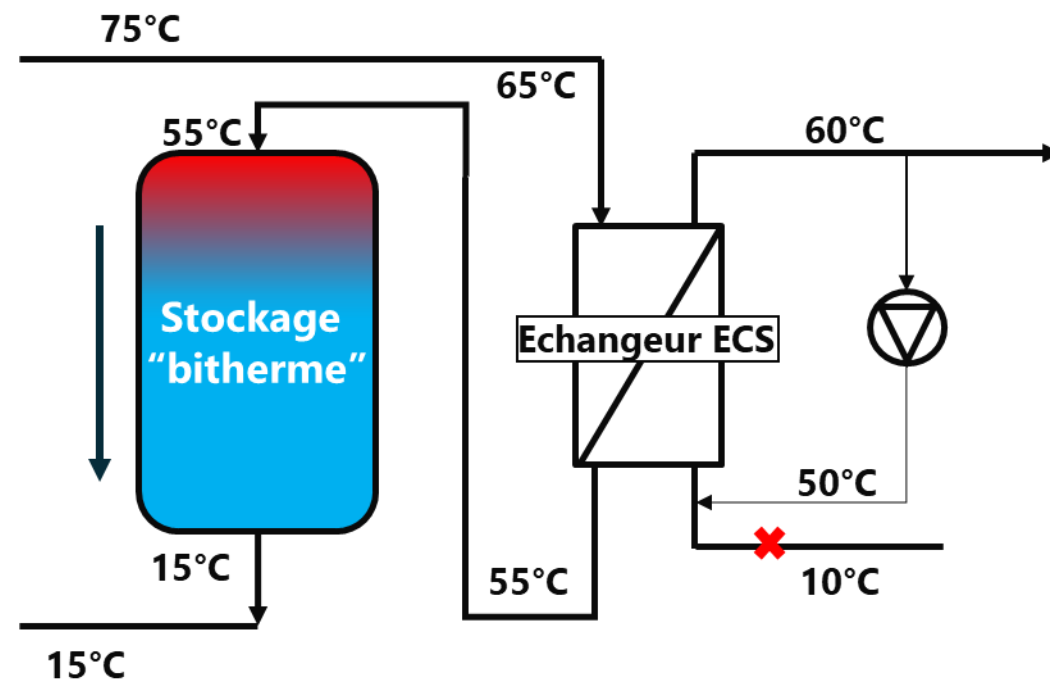
Mode Production ECS



- Vidange du chaud à 55°C du ballon
- Remplissage de froid à 15°C du ballon

⇒ Lissage de l'appel de puissance

Mode Bouclage sanitaire seul

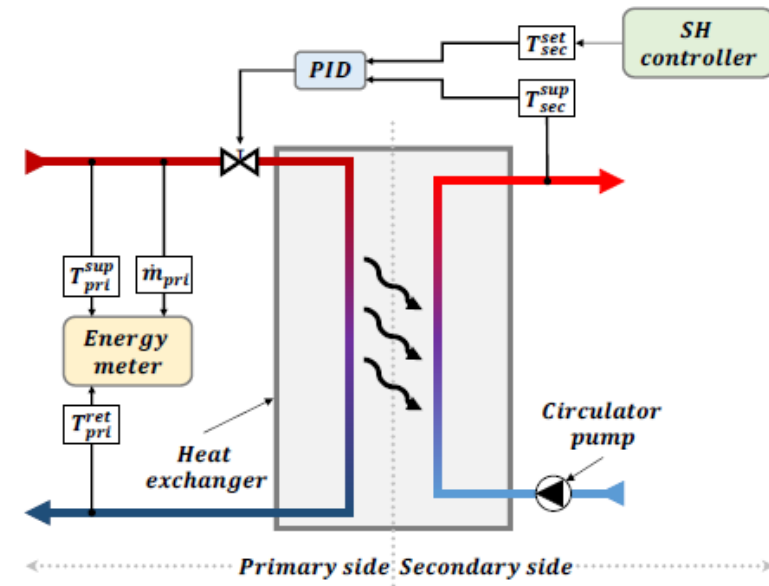


- Vidange du froid à 15°C du ballon
- Remplissage de chaud à 55°C

⇒ Diminution température de retour

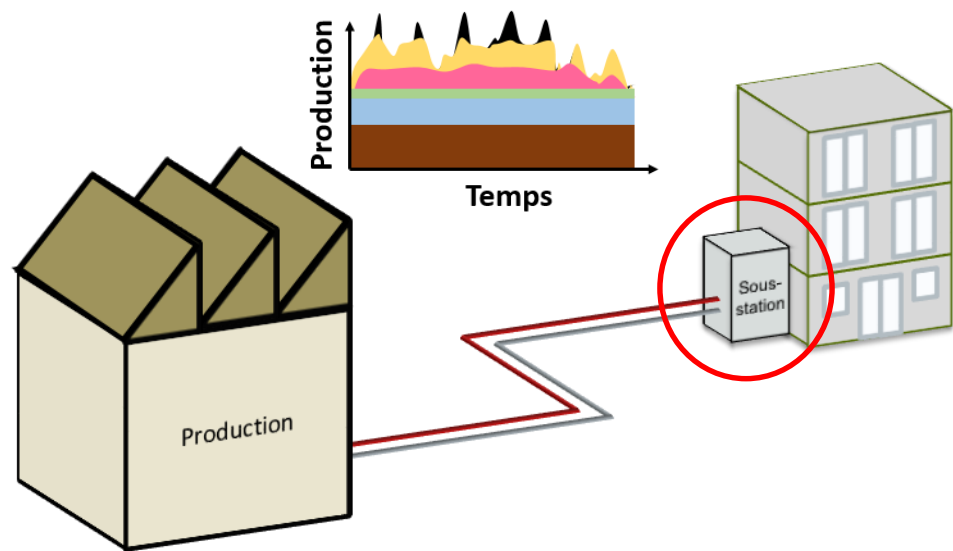
TOPIC 4:

Advanced Control



Limit loads on the production plants

Demand-Side Management

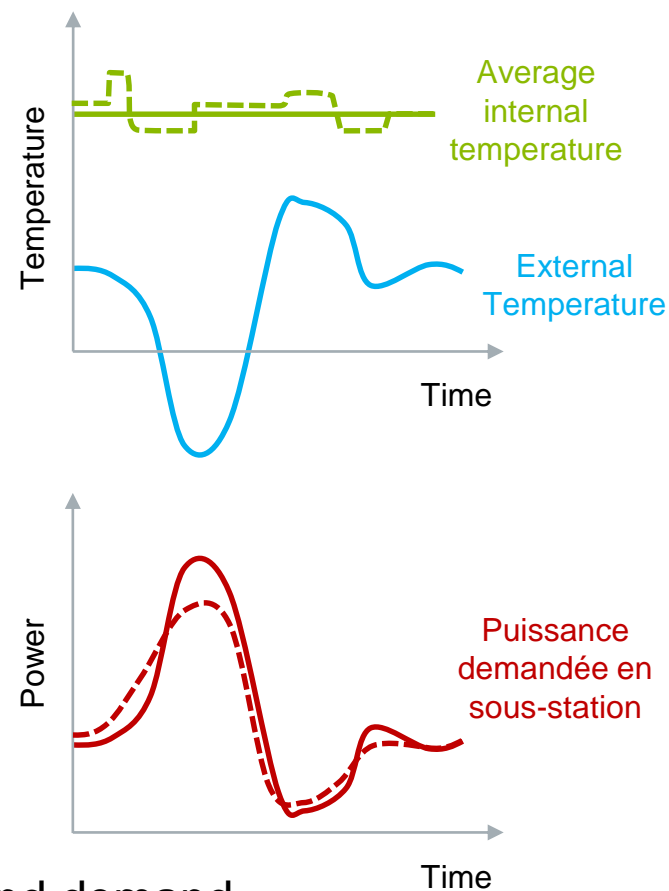


Advanced management (Predictive control)

Prediction of
consumption on
the horizon

Optimization of the load
under internal temperature
constraints

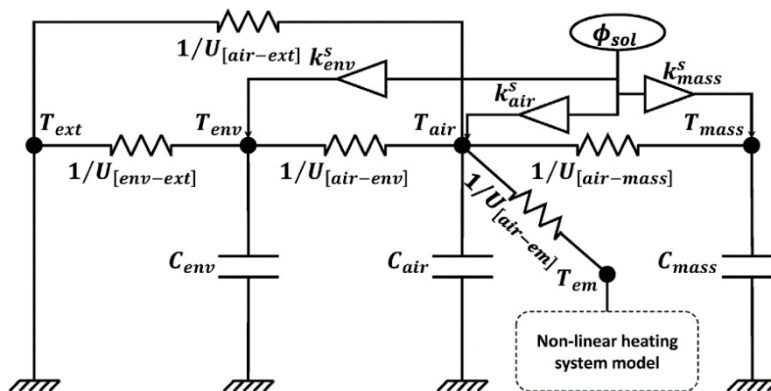
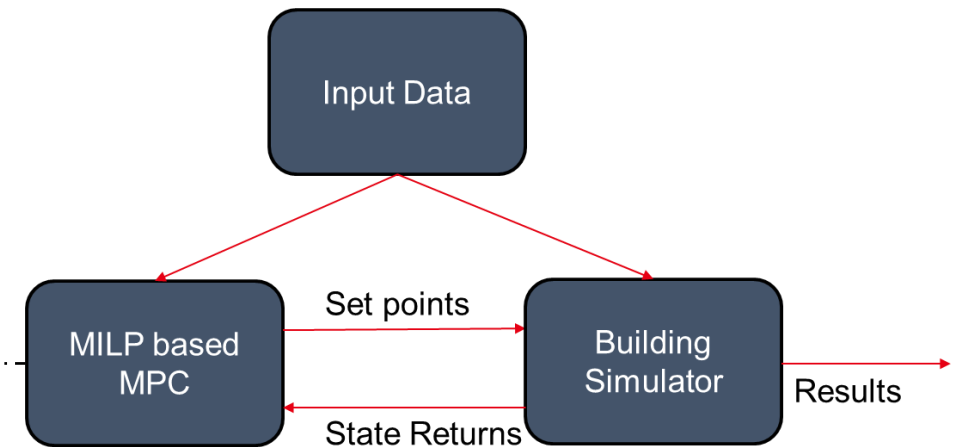
Advanced Control



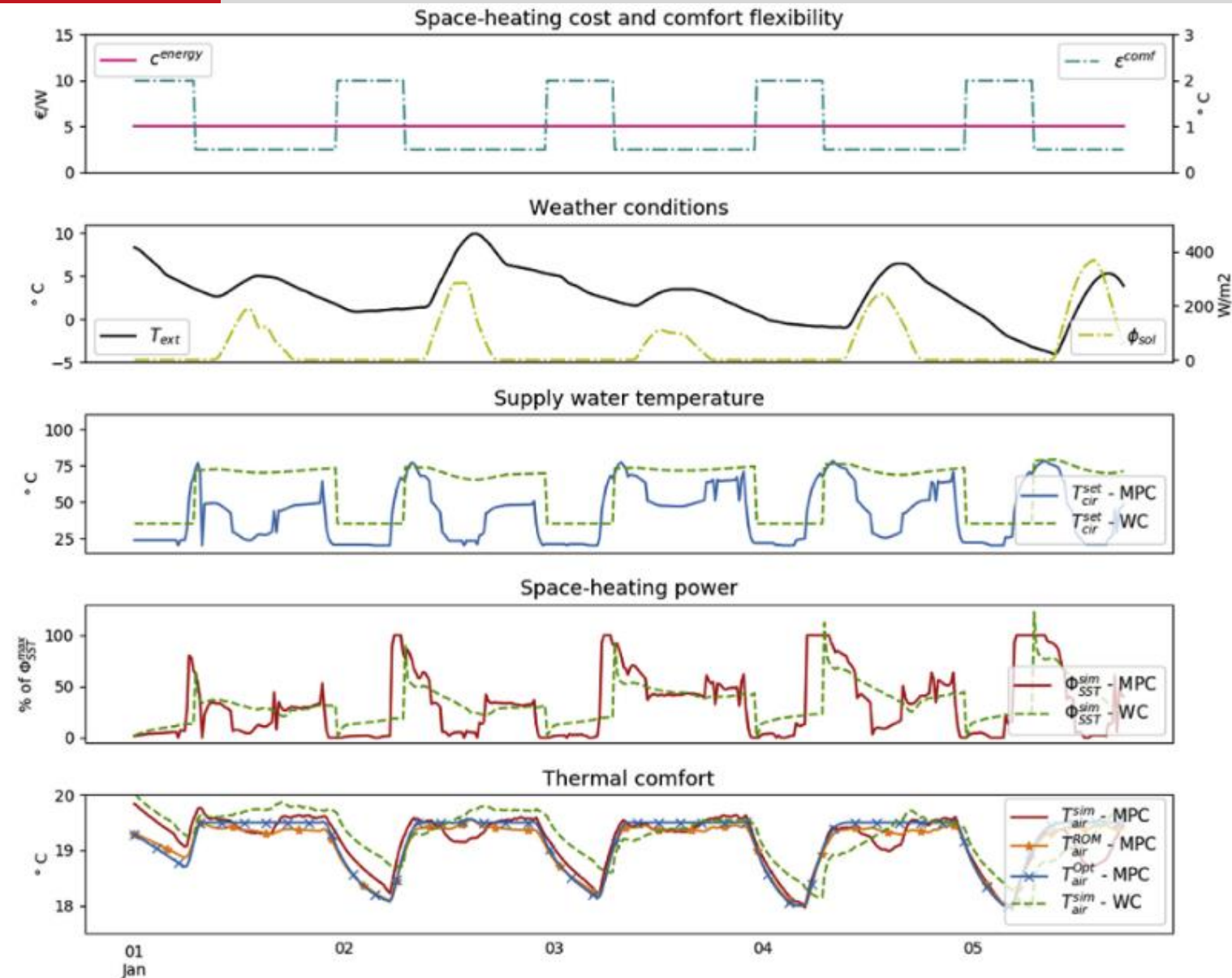
➡ Towards combined optimization of production, distribution and demand

- MILP based MPC for SH demand
- Use of Heating circuit and internal mass for flexibility
- Replacement of WC with demand-side management

3rd order ROM model
 Non linear heating circuit model → linearized for MPC
 16 parameters identified with detailed model
 Identification use data available at the SST (power, flow, T setpoint)



$$f_{obj} = \sum_{n=1}^N \left(\begin{aligned} &p^{energie}[n] \cdot Q_{SST}[n] \cdot \Delta t \\ &+ p^{sur-chauffe}[n] \cdot \Delta T_{air}^{sur-chauffe}[n] \cdot \Delta t \\ &+ p^{sous-chauffe}[n] \cdot \Delta T_{air}^{sous-chauffe}[n] \cdot \Delta t \\ &+ p^{pertes}[n] \cdot \Delta T_{cir}^{pertes}[n] \cdot \Delta t \end{aligned} \right)$$



Standard WC control using a static heating curve with a night-time set-back limiting $T_{\text{set, cir}}$ to 35°C from 11:00 p.m. to 6:45 a.m., $T_{\text{set, air}} = 19.5^\circ\text{C}$

VS

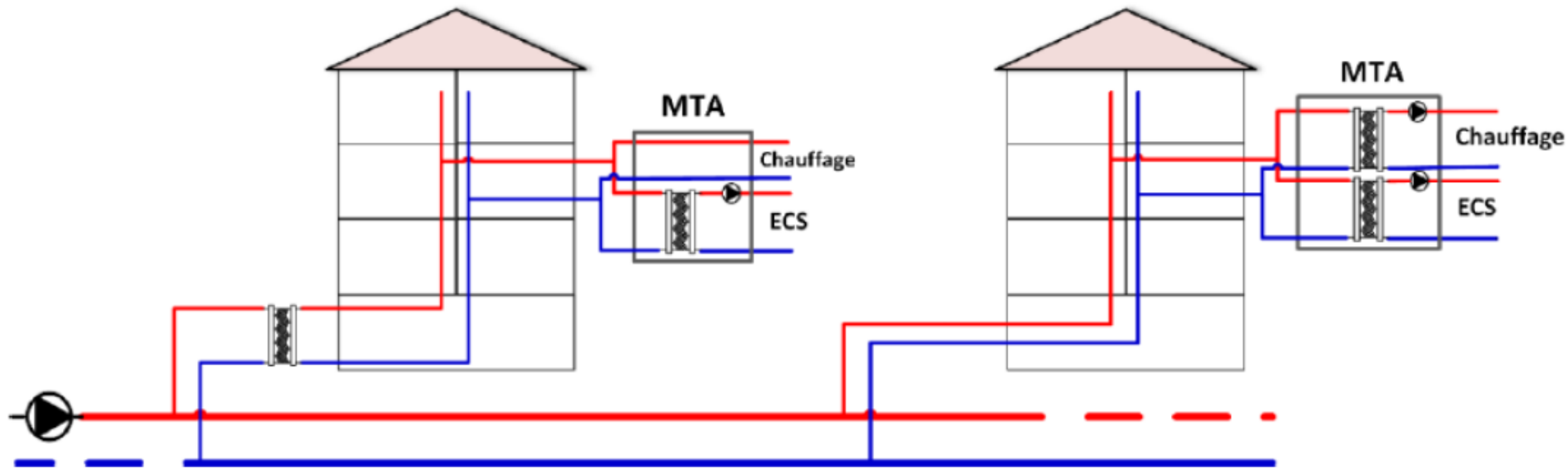
MILP-based MPC considering fixed energy cost with $\epsilon_{\text{comf}} = 0.5^\circ\text{C}$ during the day and $\epsilon_{\text{comf}} = 2^\circ\text{C}$ from 11:00 p.m. to 6:45 a.m.,

RESULTS

- Reduced supplied water temperature exploiting at best the 2°C flexibility and anticipates solar gains
- MPC launches and exists set back period ahead because anticipation of thermal inertia
- Peak-shaving not achieved with constant energy cost

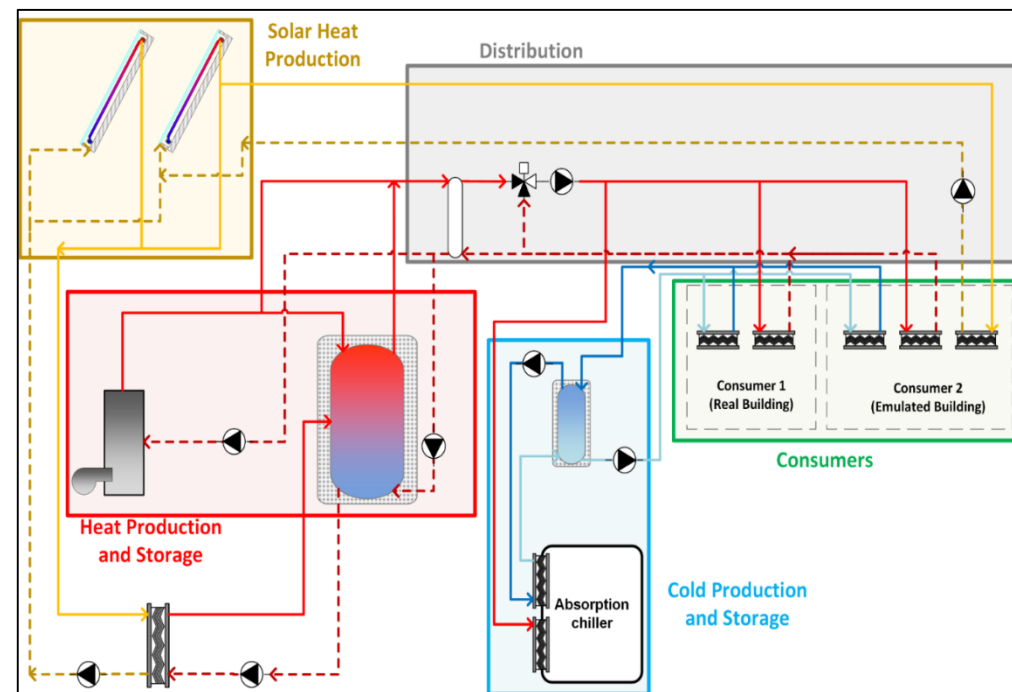
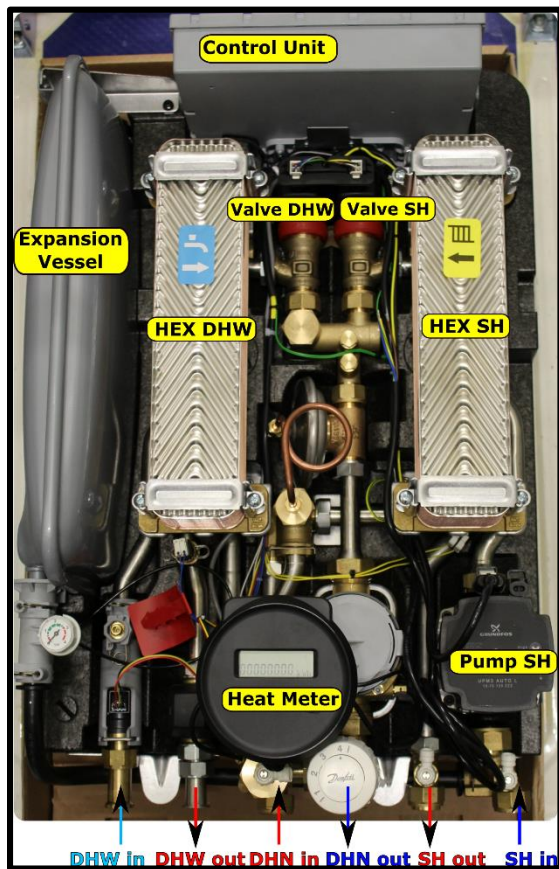
TOPIC 5:

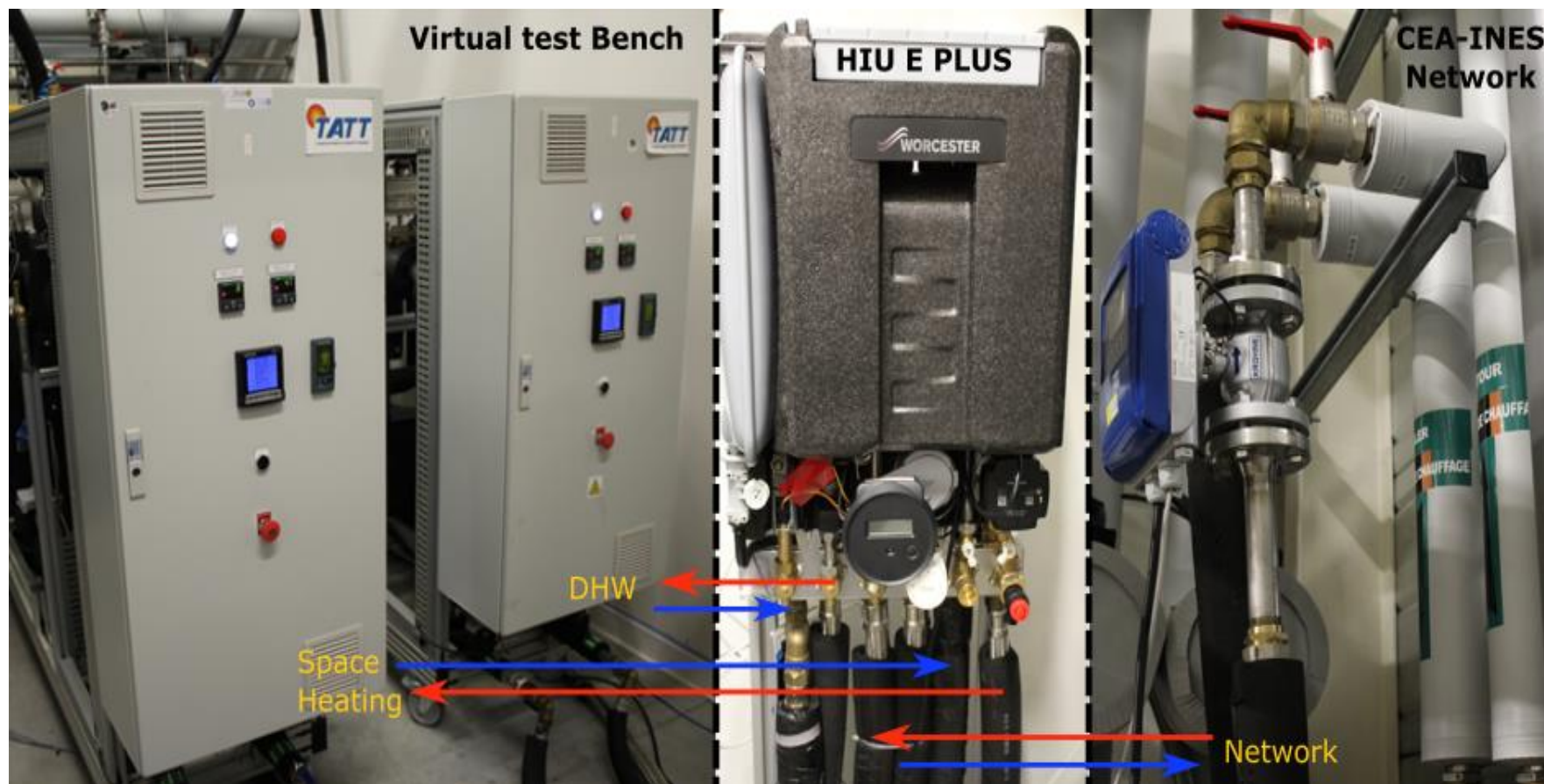
Apartment Substation



With an individual substation, the secondary side return temperature is the smallest as possible because component sized for a single user.

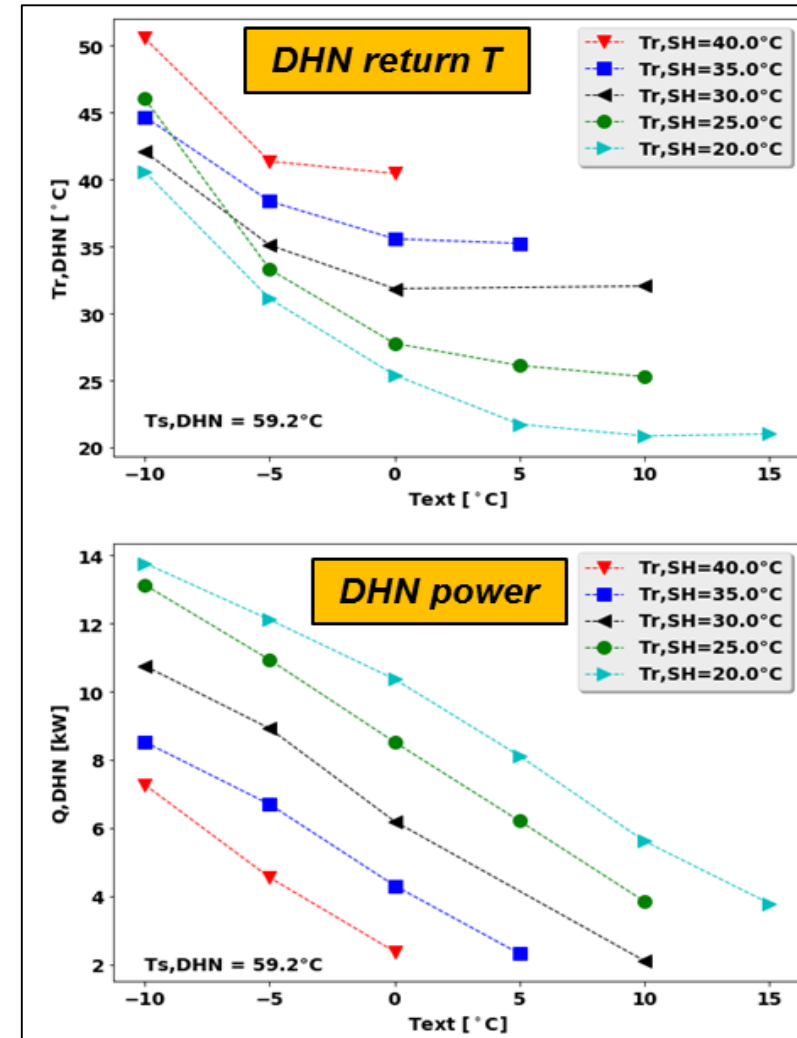
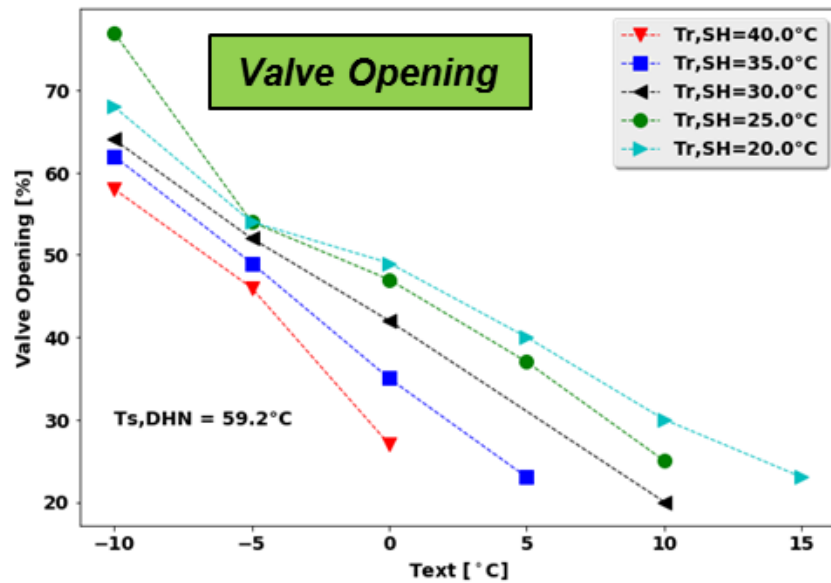
DHN return temperature is thus further reduced



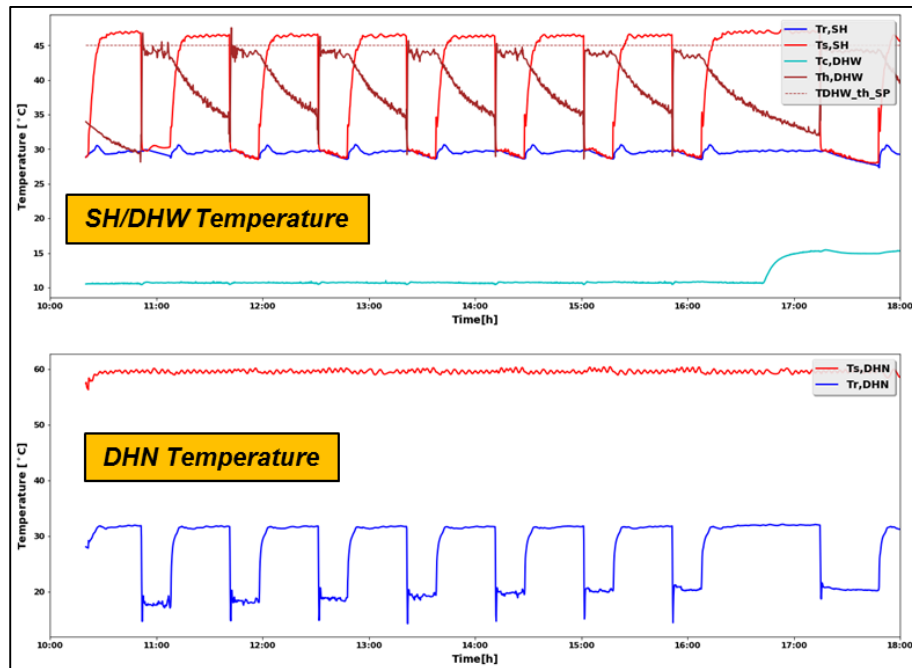


Validation TESTS

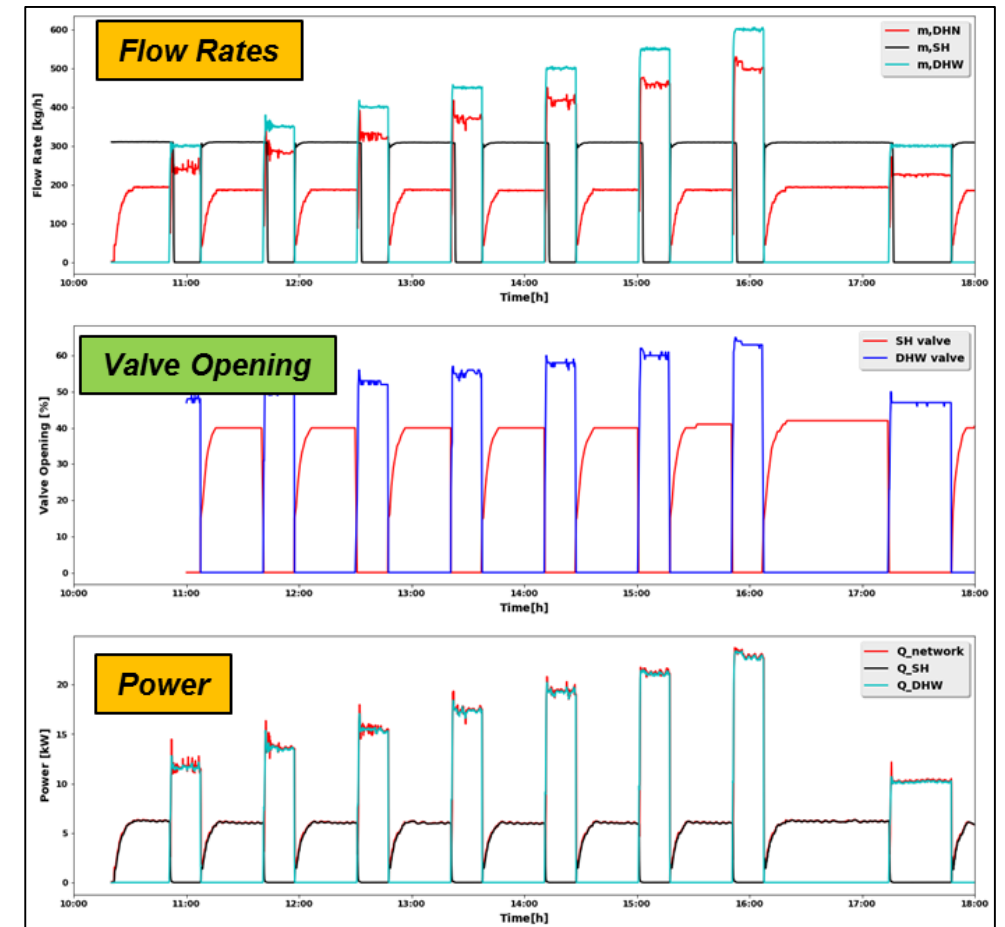
Space Heating Only (STEADY)



Validation TESTS - Dynamic



- Sudden change of return T at each draw-off
- Very fast DHW response time (less than 1 minute with only a slight overshoot)
- DHW priority



TOPIC 6:

Faults in Substation

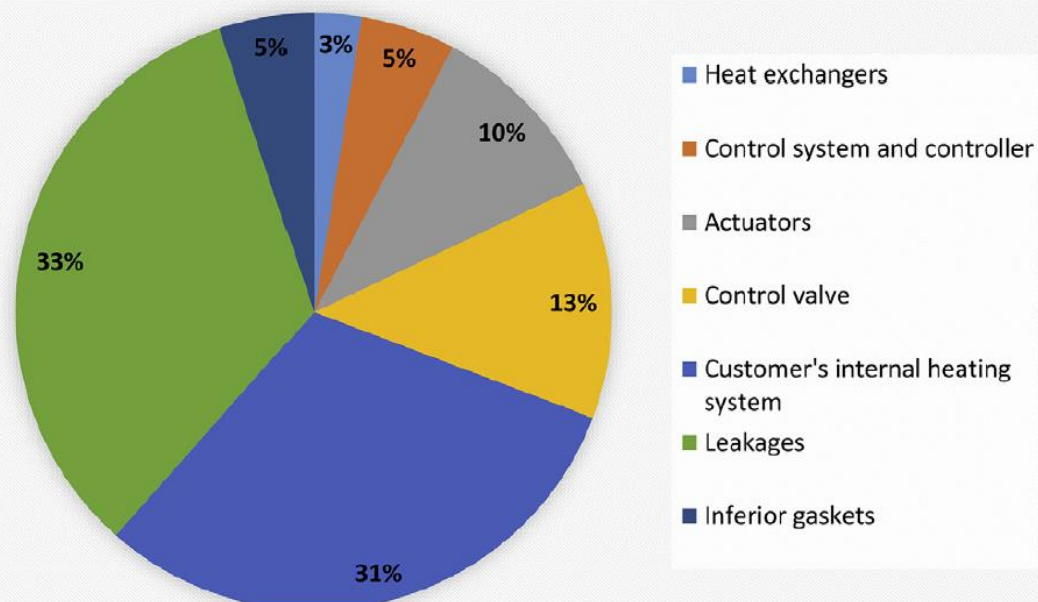
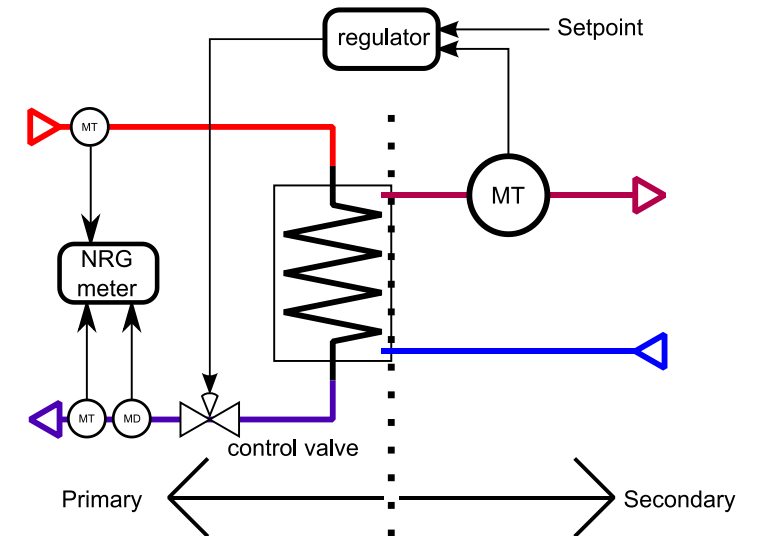
Implement at fine sampling a digital monitoring

Focus is on the problem of high return temperature:

- Short circuit flows (intentional and non-intentional)
- Too low supply temperatures in peripheral substations
- Errors in substation
- Errors in customer heating system

➔ Detection and priority set using overflow indicator

« District Heating And Cooling », S. Frederiksen and S. Werner, Studentlitteratur, Sweden, 2013



Mansson et al., *Faults in district heating customer installations and ways to approach them: Experiences from Swedish utilities*, Energy, 2019

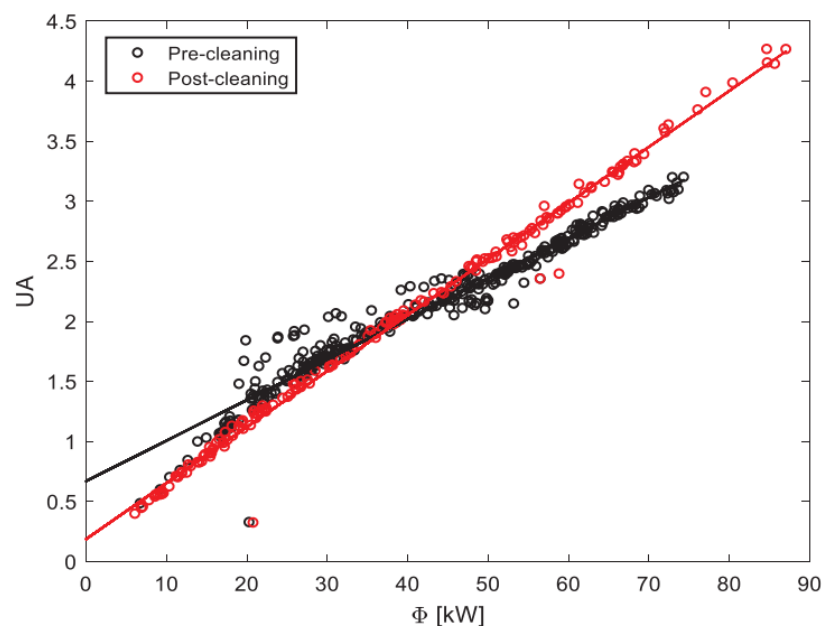
3 different fault groups:

- Unsuitable heat load patterns
 - Low average return temperature
 - Poor substation control
- ➔ Use of automatic data collection is necessary

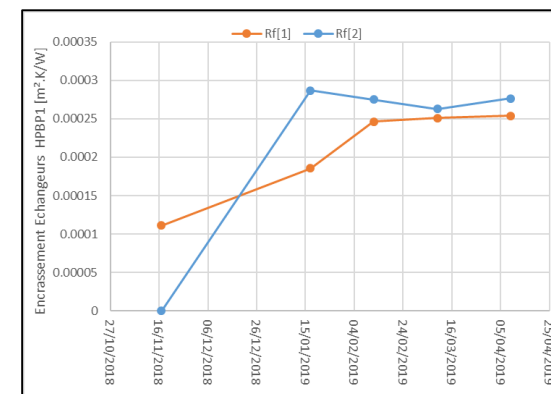
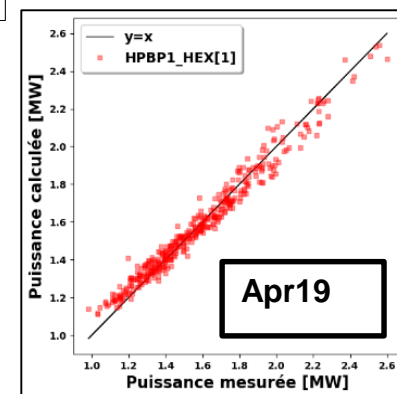
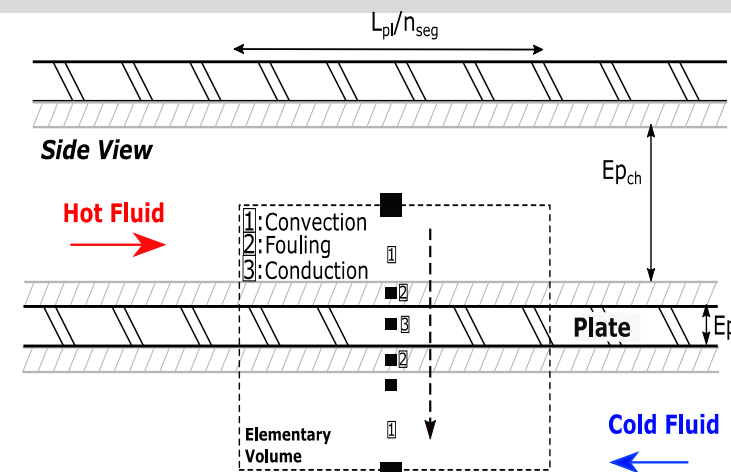
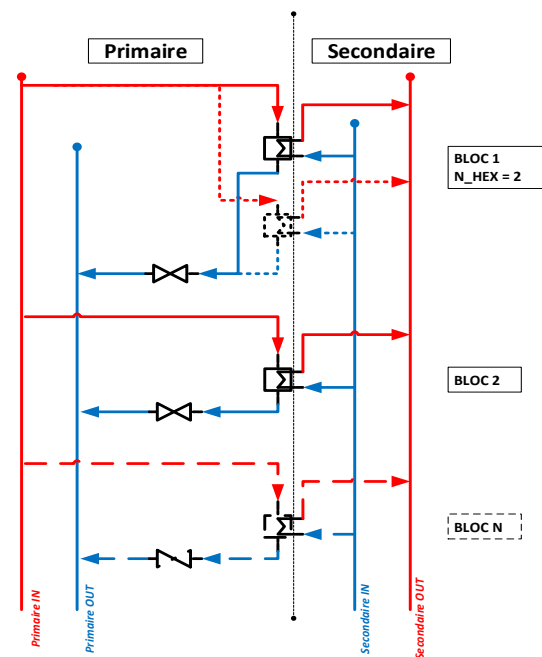
Gadd and Werner, "Fault detection in district heating substations", Applied Energy, 2015

Fouling detection using:

- full substation model and identification of the fouling parameter
- steady state detection and linear fit of Q as a function of UA :
assumption of constant DTLM



→ If slope increases, HEX is fouled



THANKS FOR YOUR ATTENTION

Commissariat à l'énergie atomique et aux énergies alternatives
17 rue des Martyrs | 38054 Grenoble Cedex
www-liten.cea.fr

Établissement public à caractère industriel et commercial | RCS Paris B 775 685 019